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## National Water Research Institute

Final Report on

### Assessing the Ability of the Zenon ZenoGem® Membrane Bioreactor to Meet Existing Water Reuse Criteria

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September 2001

# **FINAL REPORT**

**National Water Research Institute**

## **Assessing the Ability of the Zenon Zenogem<sup>®</sup> Membrane Bioreactor to Meet Existing Water Reuse Criteria**

September 2001

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# **SECTION 1**

## **Introduction**

### **1.1 INTRODUCTION**

As areas around the United States and the world have seen an increased need for the use of reclaimed wastewater this has encouraged the development and implementation of new wastewater reclamation technologies. Membrane bioreactors (MBR) are an example of a wastewater reclamation technology that is currently in use in countries around the world and offers greater promise for increased use in the future.

MBR combines the use of a membrane module and a separate bioreactor. Low pressure membranes, either microfilters (MF) or ultrafilters (UF), are used for the solids separation step. The membrane keeps solids and high-molecular weight compounds in the bioreactor by separating them from the treated water. Sludge concentration in the MBR is controlled by continuous liquid extraction from the bioreactor. As sludge concentration and hydraulic retention time are dissociated in the MBR process, good control of biological processes can be achieved and a high water quality effluent produced. MBR therefore, combines the process elements of secondary, tertiary and advanced wastewater treatment into a single unit operation.

There are two basic configurations of MBR unit processes. They can either be operated “in-series” or “submerged” (Adham, 1998). In the “in-series” configuration, sludge is pumped from the aeration basin to a pressure driven membrane system outside of the bioreactor where the suspended solids are retained and recycled back into the bioreactor. The effluent passes through the membrane. In this configuration, the membranes are regularly backwashed to remove suspended solids build-up and accumulations and are chemically cleaned when operating pressures become too high.

In the “submerged” configuration, a low pressure membrane is submerged in an aeration basin and operated under vacuum. The membrane is agitated by coarse bubble aeration that helps



prevent suspended solids accumulation at the membrane surface. Submerged membranes are either regularly backwashed or relaxed and are chemically cleaned when the operating pressures become too high.

## **1.2 BUREAU OF RECLAMATION STUDY**

In October 1998 the City of San Diego was awarded a grant from the Bureau of Reclamation to evaluate the MBR and its potential application to wastewater reclamation. During the study, the City of San Diego and their consultant, MWH, performed a parallel comparison of the two leading manufacturers of MBR. This report includes the results and observations for the study conducted using the Zenon MBR process. An overview of the materials and methods for the pilot-plant study is presented in Section 2 of this report.

During Part 1 of the testing, the system was operated in a nitrification/denitrification mode using an auxiliary anoxic tank. During Part 2, the pilot plants were operated in a nitrification only mode. The primary objectives of the Bureau of Reclamation project were to obtain long-term operational and performance measures for the MBR process in treating primary wastewater effluent. An overview of the results from the Bureau of Reclamation study are provided in Section 3 of this report.

## **1.3 NWRI PROJECT OBJECTIVES**

During the Bureau of Reclamation funded study, preliminary research and contacts were made into what would be necessary to obtain regulatory approval for the use of MBR to meet California's Title 22 Water Recycling Criteria. This NWRI study builds on that initial work with the primary focus of the NWRI project to develop information on regulatory requirements for wastewater reclamation and obtain, if possible, approval from selected State agencies for the use of MBR technologies in meeting their water reclamation criteria.

During initial contacts with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process, DHS staff requested additional data

showing the ability of the MBR process to remove viruses. As part of the NWRI project, therefore, virus seeding experiments were conducted to provide that needed information.

#### **1.4 VIRUS SEEDING EXPERIMENTS**

Virus seeding experiments were performed under various fouled conditions (low, medium and high) using both primary wastewater effluent and Colorado River Water (CRW). The results of the virus seeding experiments are presented in Section 4 of this report.

#### **1.5 STATE REGULATORY REQUIREMENTS**

In addition to California DHS, contacts with state regulatory agencies were made in Arizona, Florida, Oregon, Texas and Washington. Discussions were held to identify state regulations regarding wastewater reclamation criteria and the possibility of obtaining some kind of formal feedback and/or approval regarding the use of the MBR process. Regulators in each state received copies of the California DHS approval letter and the report to NWRI that presented a summary of the Bureau of Reclamation MBR study and subsequent virus seeding study. A cover letter requested review of the materials and a written response with regard the capabilities of the system in meeting state wastewater reclamation requirements. The results of this effort are presented in Section 5 of this report.

## SECTION 2

### Materials and Methods

#### 2.1 FEED WATER CHARACTERISTICS

The virus seeding experiments were conducted using both primary effluent wastewater and fresh water. The municipal primary effluent wastewater was from the San Pasqual Water Reclamation Plant (SPWRP). This was the same municipal primary effluent wastewater used during the main study investigating the performance of the MBR. The primary treatment processes were a travelling screen, a vortex grit chamber, a rotary drum screen, and a rotary disc filter. Table 2-1 shows water quality of the primary effluent wastewater that the MBR pilot plant treated during the Bureau of Reclamation study. When the virus seedings were performed using fresh water, Colorado river water (CRW) was used for all experiments. Table 2-2 shows representative water quality of CRW.

**Table 2-1 Primary effluent water quality during Bureau of Reclamation pilot study**

	No. of Analyses	Units	Median	Maximum	Minimum
Ammonia-N	5	mg/L	28.7	37.7	1.9
Nitrate-N	7	mg/L	ND	ND	ND
Nitrite-N	4	mg/L	0.01	0.03	ND
TKN	8	mg/L	32.4	59.6	15.6
Ortho-Phosphate-P	7	mg/L	3.59	4.24	2.95
Total Phosphorus	7	mg/L	7.04	8.57	4.68
Bromide	8	mg/L	0.24	0.30	0.18
Chloride	8	mg/L	160	173	141
Sulfate	8	mg/L	162	180	142
BOD <sub>5</sub>	20	mg/L	72	102	38
DOC	22	mg/L	11.3	24.8	8.9

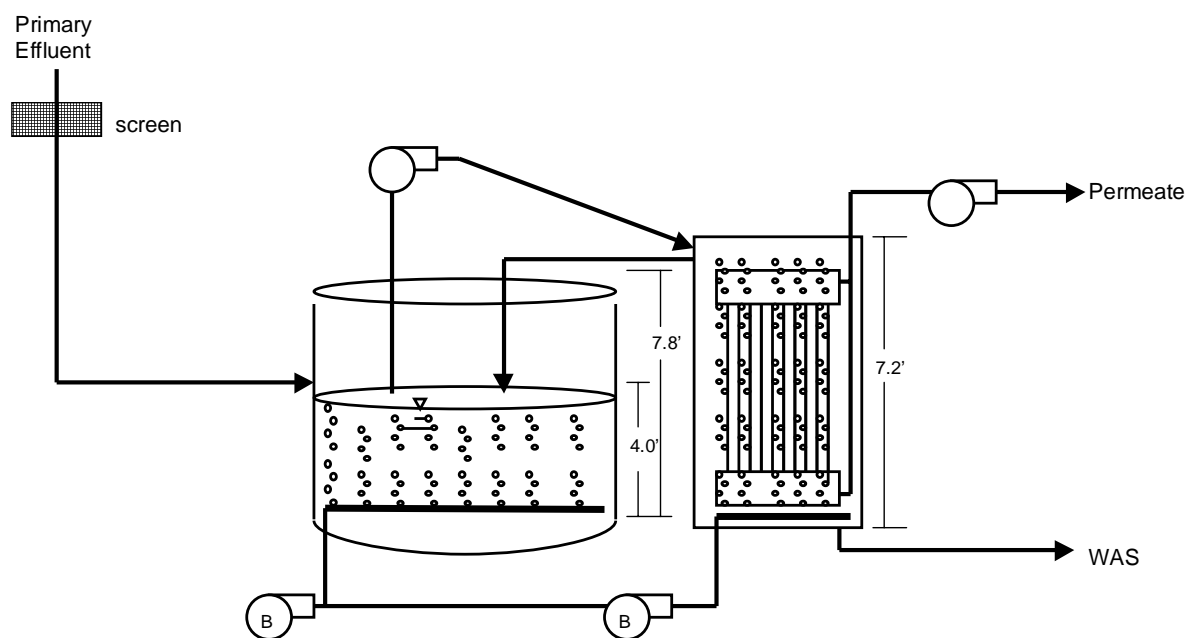
**Table 2-2 Representative water quality for Colorado River Water**

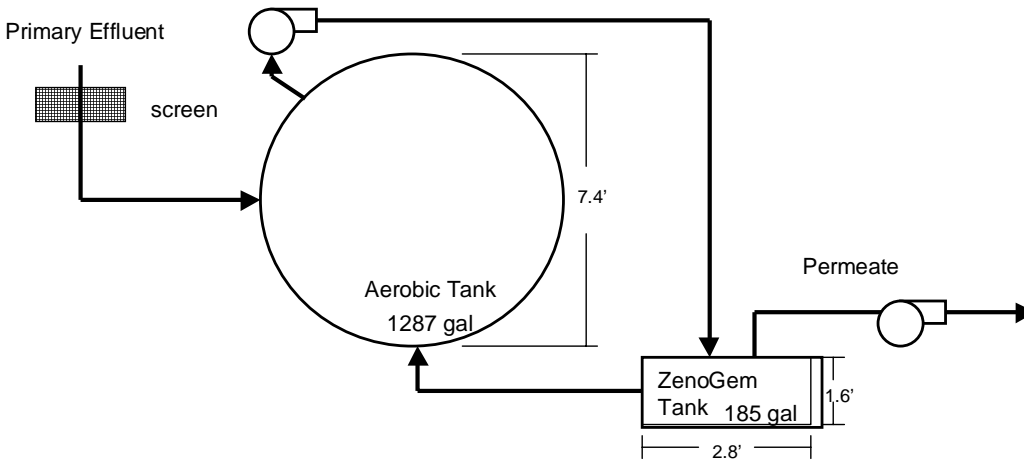
	No. of Analyses	Units	Median	Maximum	Minimum
Alkalinity	5	mg/L as CaCO <sub>3</sub>	120	130	120
Total Hardness	5	mg/L as CaCO <sub>3</sub>	240	240	220
Calcium Hardness	4	mg/L as CaCO <sub>3</sub>	150	160	140
Total Suspended Solids	5	mg/L	10	15	1.8
Total Dissolved Solids	5	mg/L	500	500	490
TOC	5	mg/L	3.1	4.1	2.5

## 2.2 DESCRIPTION OF PILOT PLANT

The Zenon MBR pilot unit was equipped with a 1,287-gal (4.87 m<sup>3</sup>) aerobic tank and a 185-gal (0.7 m<sup>3</sup>) ZenoGem pilot unit. The MBR was fed with 3-mm screened primary effluent by a PLC-controlled submersible pump, placed in the primary effluent break tank.

One membrane cassette was submerged in the ZenoGem tank where it was agitated with coarse bubble air diffusers. A schematic of the Zenon MBR pilot unit during the testing is shown in Figure 2-1. The hollow fiber of the Zenon OCP ultrafilter (UF) membrane consisted of a total surface area of 519 ft<sup>2</sup> (48 m<sup>2</sup>). The hollow fibers are arranged vertically and attached at both ends to a top and bottom header. The membrane is operated under vacuum pressure. The specifications of the Zenon membrane is given in Table 2-3. The Zenon membrane was initially operated at a flux = 19 gfd (32 L/h-m<sup>2</sup>) and a coarse bubble airflow = 30 scfm (0.8 m<sup>3</sup>/min). The coarse bubble aeration was initially operated consistently. During Part 2, the aeration was operated on a cycle of 10 s on, 10 s off. After demonstrating acceptable performance under these conditions, the flux was increased to 21 gfd (36 L/h-m<sup>2</sup>) and the airflow remained the same. The membrane was operated using cycle of a 10 min production and a 15 s backwash, when membrane was backwashed using product water.





**Figure 2-1 Zenon MBR side view (top) and plan view (bottom)**

**Table 2-3 Specification for the Zenon OCP Ultrafiltration Membrane**

	Units	Value (OCP Membrane)
Approximate Size of Element (L x W x	mm	2 x 0.75 x 0.2
Active Membrane Area	ft <sup>2</sup> (m <sup>2</sup> )	519 (48.2)
Number of Fibers	---	~4700
Inside Diameter of	mm	0.75
Outside Diameter of	mm	1.95
Approximate Length of	m	1.65
Flow Direction	---	Outside-In
Nominal Membrane Pore	μm	0.035
Membrane	---	Proprietary
Membrane Surface	---	Hydrophilic
Membrane	---	Neutral
Recommended Design Flux	gfd (L/h-m <sup>2</sup> )	15-20 (26-34)
Approval Study Test Flux	gfd (L/h-m <sup>2</sup> )	19 (32)
Acceptable Range of Operating pH	---	5-9 (cleaning range 2-10.5)
Vacuum Pressure for System	psi (bar)	-1 to -8 (-0.07 to -0.55)

## 2.3 CALCULATION OF OPERATING PARAMETERS

### 2.2.1 Flux Calculation

The flux of the MBR membranes can be calculated as follows:

$$J = \frac{Q_p \times 1440}{A} \quad (1)$$

Where,

J = Membrane flux (gfd)  
A = Total membrane surface area (ft<sup>2</sup>)

### 2.2.2 Temperature Correction

Low-pressure membrane fluxes are normally adjusted to a temperature of 20°C using:

$$J @ 20^{\circ}C = J \times e^{-0.0239(T-20)} \quad (2)$$

Where,

T = Feed water temperature (°C)

### 2.2.3 Specific Flux

The specific flux is the relationship between flux and the net operating pressure as follows:

$$J_{SP} = \frac{J}{P_{Net}} \quad (3)$$

Where,

J<sub>SP</sub> = Specific flux (gfd/psi)

The temperature-corrected specific flux can be calculated using the temperature corrected flux (equation 2).

### 2.2.4 Log Removal

The log removal of virus was calculated as follows:

$$Log\ Removal = Log(c_f) - Log(c_p) \quad (4)$$

Where,

c<sub>f</sub> = virus concentration in the feed (PFU/100 mL)  
c<sub>p</sub> = virus concentration in the permeate (PFU/100 mL)

Additional details on the experimental conditions and pilot-testing can be found in the report for the Bureau of Reclamation funded study (Adham, 2000).

## **SECTION 3**

### **Summary of Results from the Bureau of Reclamation Project “Membrane Bioreactors (MBR) for Water Reclamation”**

#### **3.1 BACKGROUND**

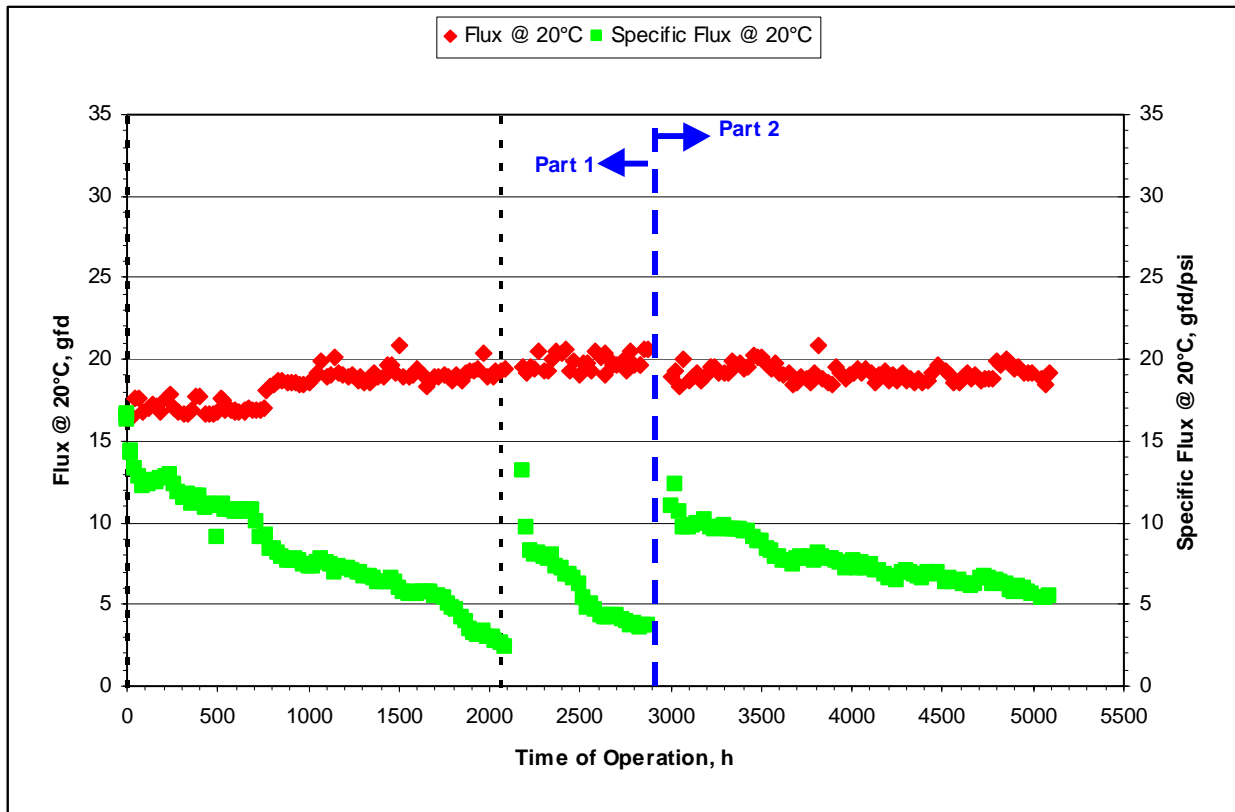
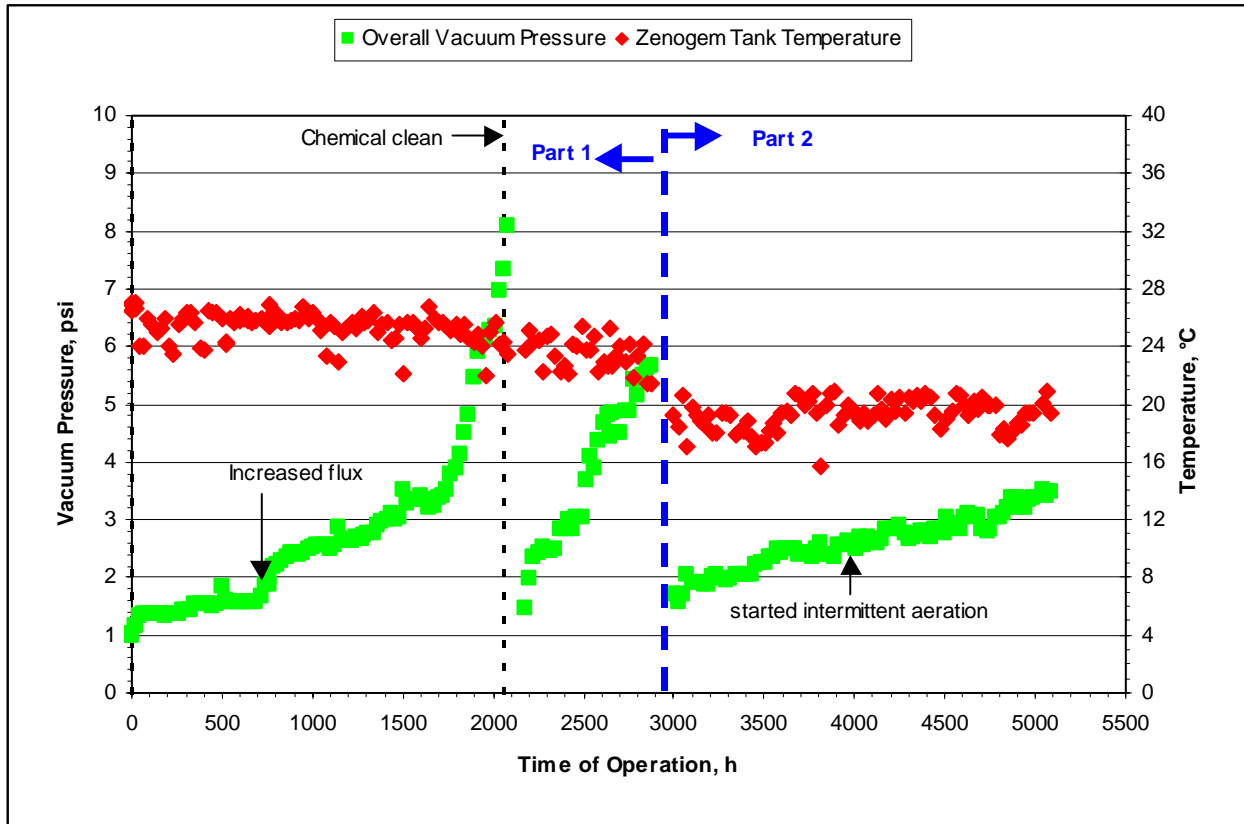
During Part 1 of the testing, the pilot plant was operated in a nitrification/denitrification mode using an auxiliary anoxic tank. During Part 2, the pilot plant was operated in a nitrification only mode. The Zenon MBR demonstrated minimal fouling throughout the testing period, producing consistent effluent turbidity values less than 0.1 NTU. The MBR produced BOD<sub>5</sub> values <3 mg/L, and up to 6-log removal of total coliforms.

#### **3.2 SUMMARY OF RESULTS**

##### ***3.2.1 Membrane Performance***

Figure 3-1 shows the membrane performance of the Zenon MBR during Part 1 and 2 of the testing. The OCP membrane ran for 2,082 h (87 d) before chemical cleaning. The chemical cleaning reduced the vacuum pressure from 8.10 psi (0.56 bar) to 1.47 psi (0.10 bar). After the chemical cleaning, the membrane ran for the remainder of Part 1, however rapid fouling was observed. Investigation into the cause of the rapid fouling of the membrane revealed that the blower airflow in the ZenoGem tank had decreased because of a blower malfunction, and the decrease in airflow corresponded to the rapid fouling events.

At the end of Part 1 of the pilot testing, the MBR was shut down and retrofitted to operate in a “nitrification-only” mode. The anoxic tanks were taken out of service, and the membrane was chemically cleaned before beginning Part 2 of the pilot testing. The Zenon MBR was soaked overnight in a 2,000 mg-NaOCl/L solution, followed by a citric acid soak overnight. During Part 2, the pilot unit was operated for 1,007 h (42 d) under continuous aeration to observe its trend of fouling trend. After this, intermittent aeration was started, and the fouling trend appeared to be unaffected by the use of intermittent aeration. The membrane ran without chemical cleaning for a period 2,087 h (87 d) during which the vacuum pressure increased from 1.72 psi (0.12 bar) to 3.49 (0.24 bar) psi.

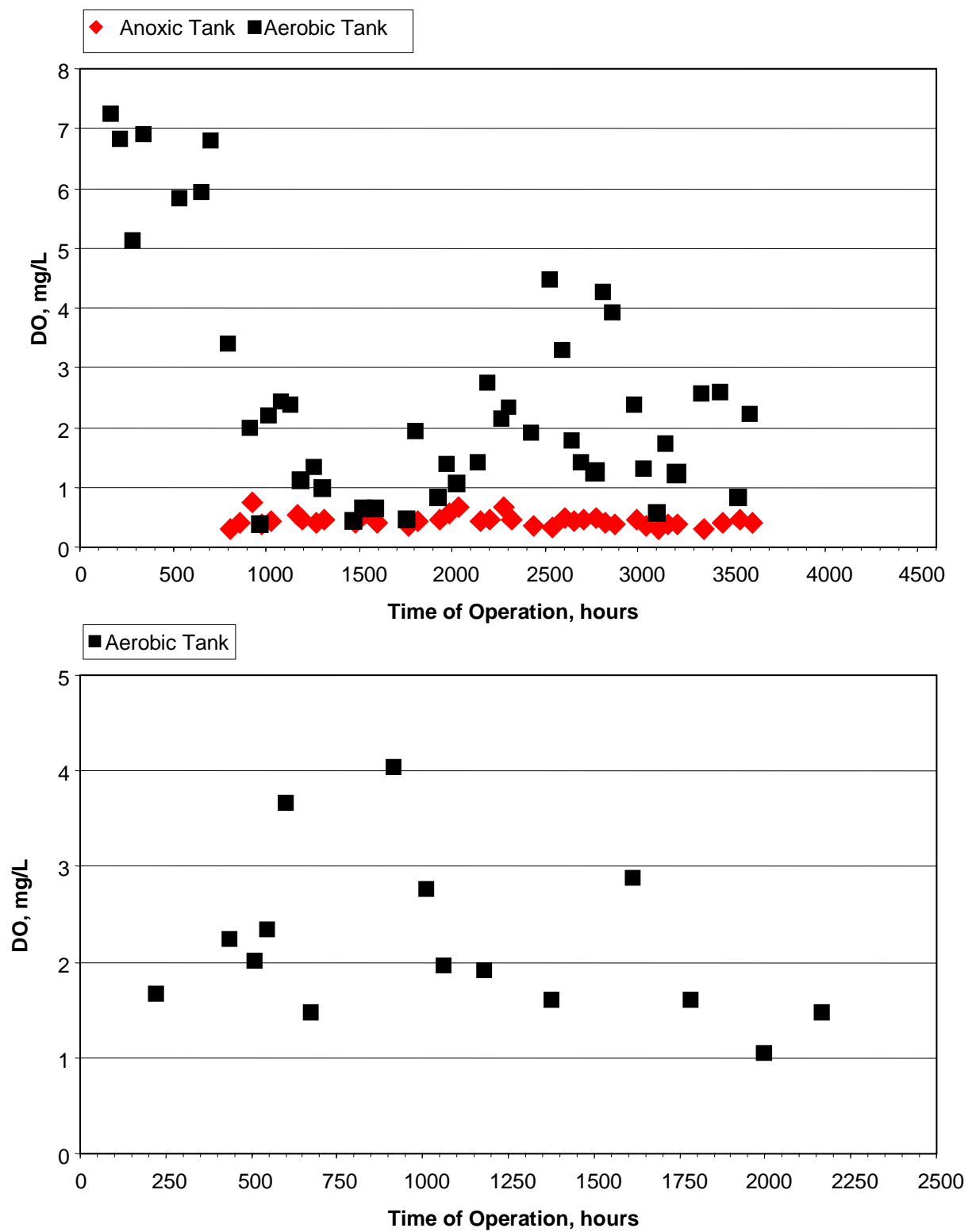


**Figure 3-1 Membrane Performance by the Zenon MBR**



### 3.2.2. *Dissolved Oxygen*

Concentrations of dissolved oxygen during testing of the Zenon MBR are presented in Figure 3-2. Dissolved oxygen concentrations in the aerobic and anoxic tank during Part 1 of the testing are presented in the top figure. Concentrations in the anoxic tank during Part 2 testing are presented in the bottom figure. The figure shows that after startup, similar levels of dissolved oxygen (between 0.5 and 4.5 mg/L) were maintained in the aerobic tank during both test phases. The levels of dissolved oxygen in the anoxic tank during Part 1 were consistently near 0.5 mg/L.



**Figure 3-2 Dissolved Oxygen in the Zenon MBR During Part 1 (top) and Part 2 (bottom)**

### 3.2.3 Organics Removal

The Zenon MBR effluent consistently achieved BOD<sub>5</sub> values <3 mg/L in 95% of all samples throughout the entire testing period (Figure 3-3). BOD<sub>5</sub> in the primary effluent ranged from 30 mg/L to 200 mg/L while BOD<sub>5</sub> in the Zenon MBR effluent ranged from 2 mg/L to 10 mg/L.

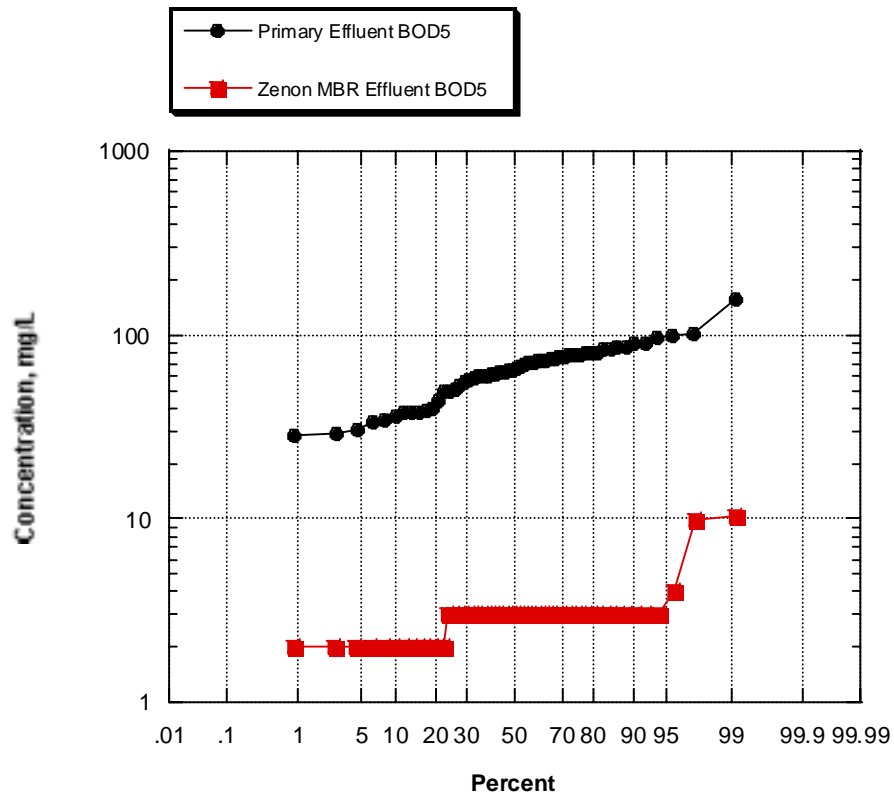


Figure 3-3 Probability plot of BOD<sub>5</sub> removal by the Zenon MBR

### 3.3.4 Particulate Removal

The Zenon MBR pilot plant produced effluent turbidity values of <0.1 NTU in 99% of the samples, as shown in Figure 3-4. Primary effluent turbidity ranged from 12 NTU to 250 NTU.

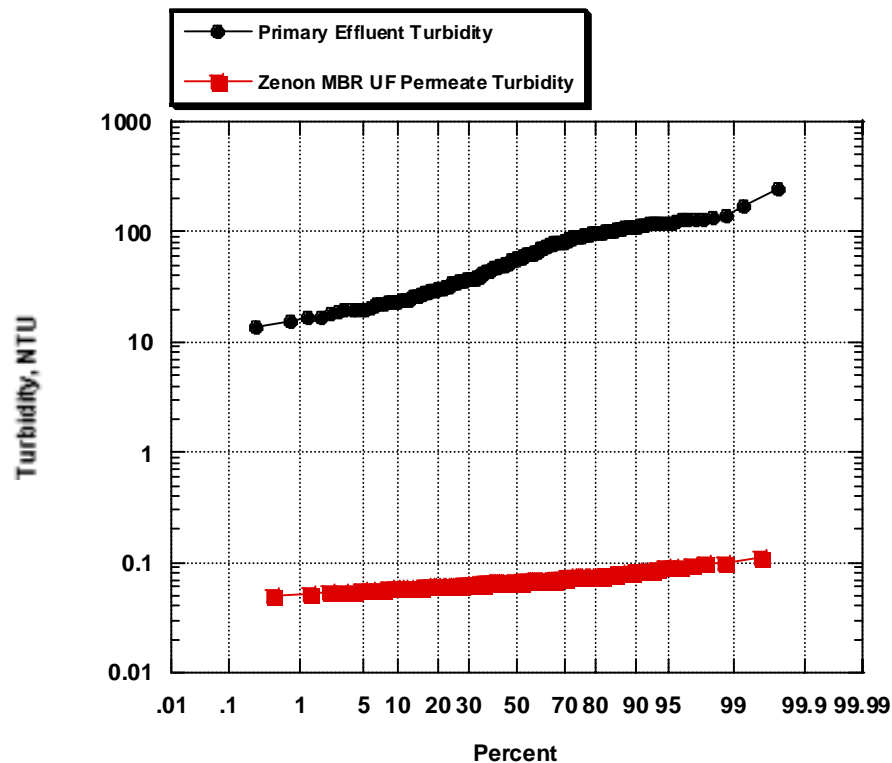
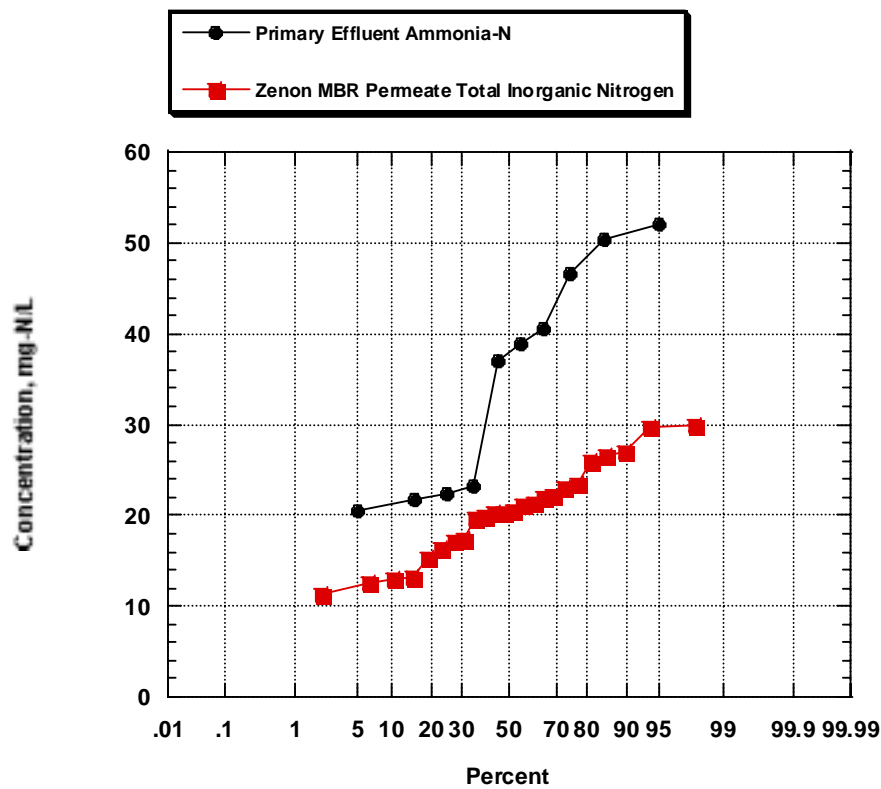
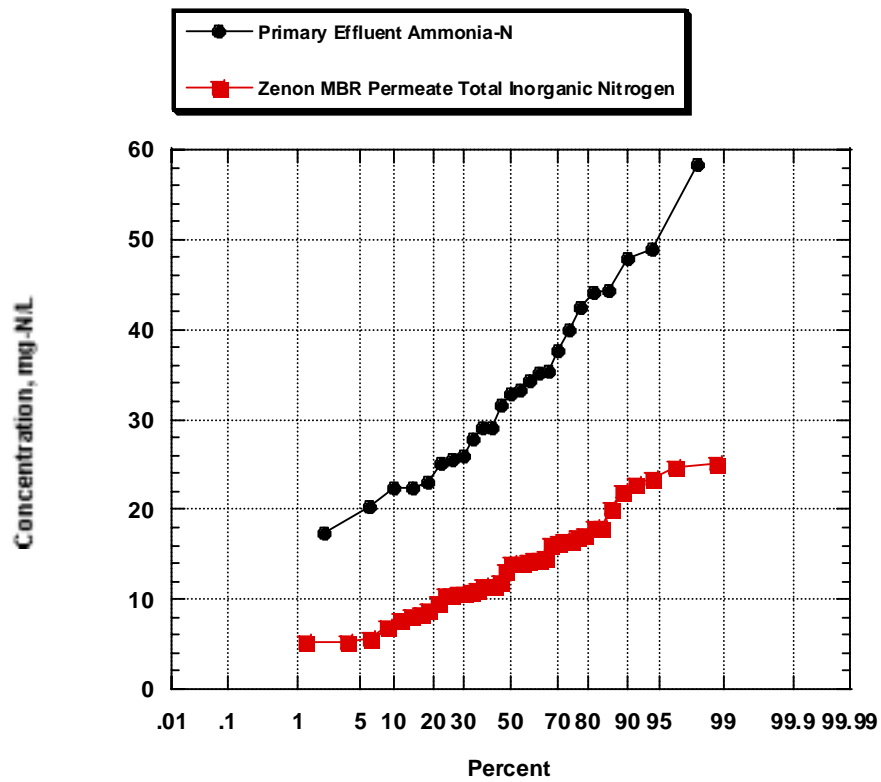


Figure 3-4 Probability plot of turbidity removal by the Zenon MBR

### 3.2.5 Biological Nutrient Removal

During Part 1 of the pilot testing, the Zenon MBR produced effluent water with total inorganic nitrogen values of <12 mg/L in 50% of all samples. (Figure 3-5) Even though nitrification and denitrification was not consistent during the testing, the MBR exhibited an ability to remove inorganic nitrogen. The aeration system and tank design were not sufficient to achieve high inorganic nitrogen removal, and this needs to be corrected in future work. The total inorganic nitrogen concentrations in the effluent during Part 1 were much lower than during Part 2. In Part 2, the effluent concentrations were <20 mg-N/L in 50 % of all samples.



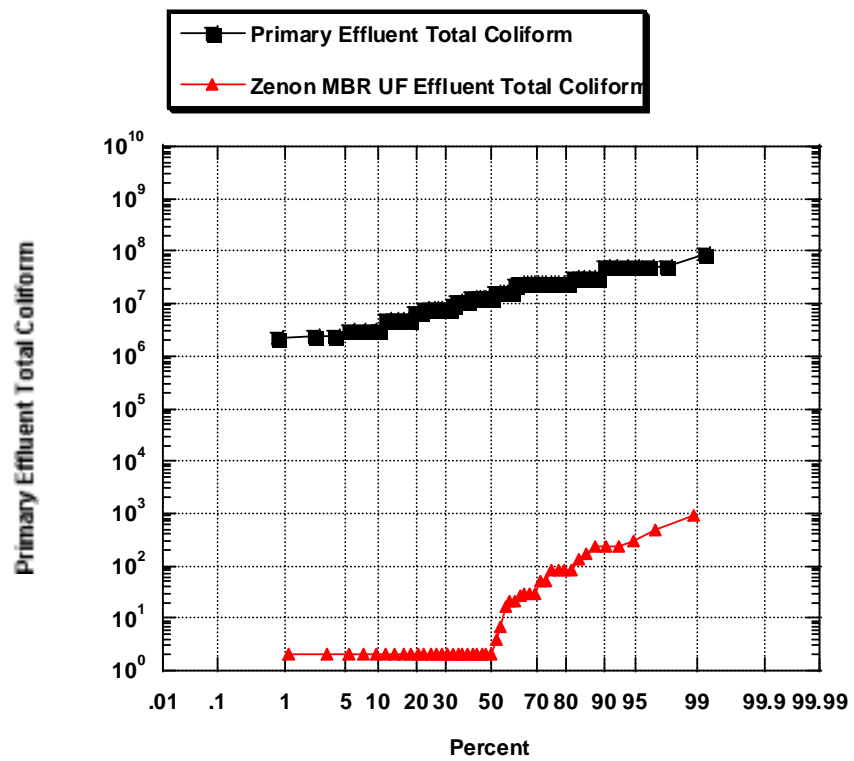
**Figure 3-5** Probability plots of the biological nutrient removal by the Zenon MBR during Part 1(top) and Part 2 (bottom)

### ***3.2.6 Total Coliform, Fecal Coliform, Total Coliphage***

The microbial concentration and log removal of the Zenon MBR can be seen in Figures 3-6, 3-7 and 3-8. The Zenon UF effluent total coliform was  $\leq 2$  MPN/100 mL in 50% of all samples while primary effluent concentrations ranged from  $2 \times 10^6$  MPN/100mL to  $1 \times 10^8$  MPN/100mL, giving >4-log removal of total coliform in 95% of all samples collected as presented in Figure 3-6.

The fecal coliform concentration of the Zenon effluent samples were  $\leq 2$  MPN/100 mL in 96% of all samples while primary effluent concentrations ranged from  $2 \times 10^6$  MPN/100mL to  $2 \times 10^8$  MPN/100mL, giving >5-log removal of fecal coliform in 95% of all samples as shown in Figure 3-7.

The effluent fecal coliphage concentration in the Zenon effluent was  $\leq 1$  PFU/100 mL in 95% of all samples while primary effluent concentrations ranged from  $4 \times 10^2$  PFU/100mL to  $3 \times 10^5$  PFU/100mL, giving 3-log removal of fecal coliphage in 95% of all samples as presented in Figure 3-8.



**Figure 3-6** Probability plot of microbial log removal by the Zenon MBR

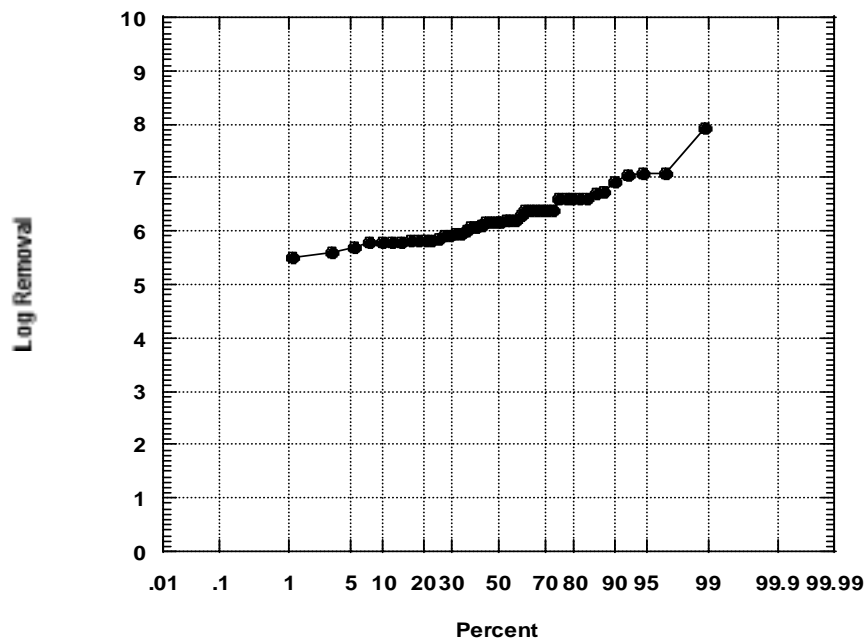
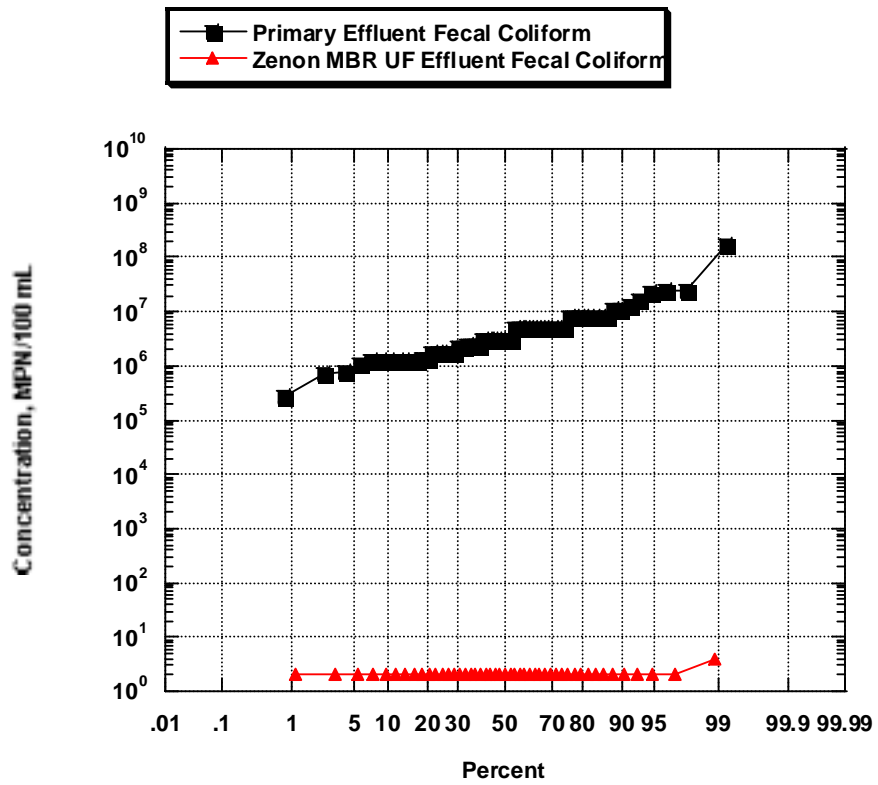


Figure 3-7 Probability plot of Fecal Coliform removal by the Zenon MBR



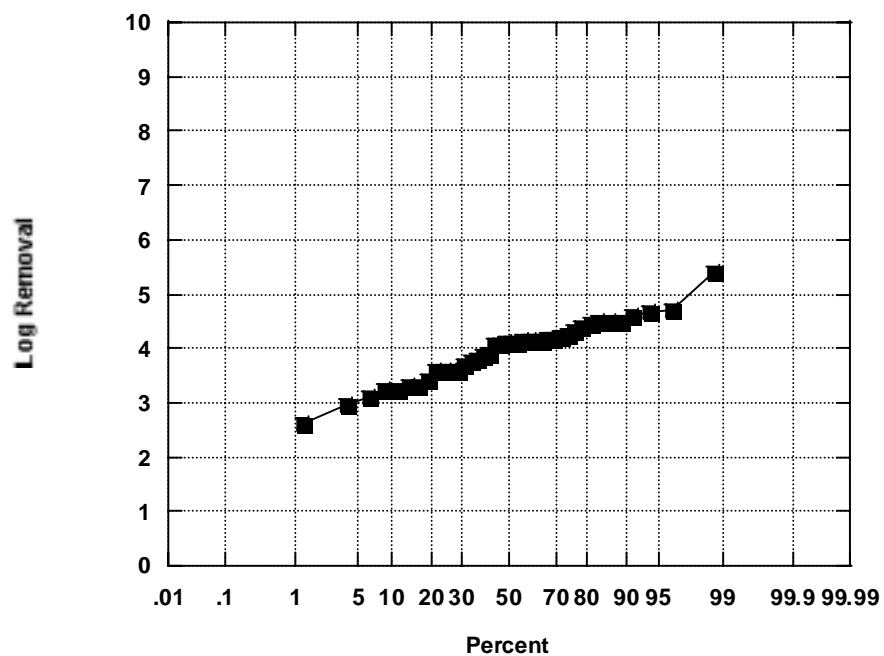
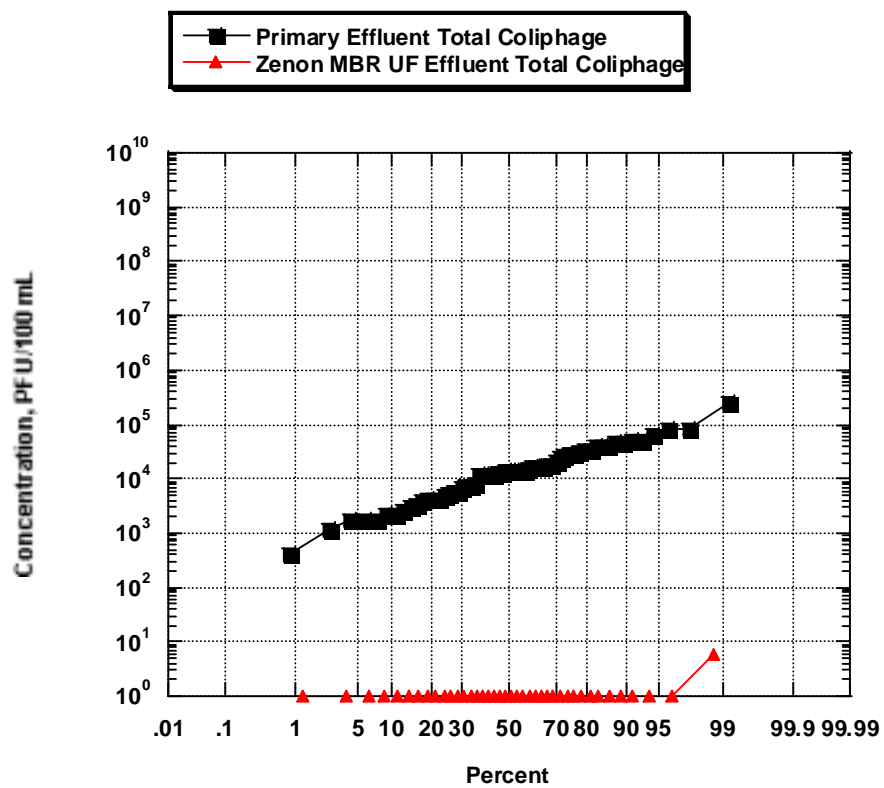


Figure 3-8 Probability plot of Total Coliphage removal by the Zenon MBR

## SECTION 4

### Summary and Results of MBR Virus Seedings

#### 4.1 VIRUS SEEDING PROTOCOL

##### 4.1.1 Introduction

As indicated previously, MWH conducted virus seeding experiments with the intent to further evaluate the potential for obtaining California DHS regulatory approval for the MBR process. The approach and method for evaluating the results were discussed during a meeting held with DHS staff. Table 4-1 summarizes the protocol that was followed during the virus seeding experiments. Appendix A presents the minutes from the March 1, 2000 meeting held with representatives from DHS. Virus seeding experiments were conducted using primary effluent as well as CRW. This section presents a description of the protocol used for the virus seeding experiments and the results that were observed.

**Table 4-1 Virus Seeding Test Sampling Protocols**

Experiment	Number of Seed Solution Samples	Number of Samples	Replicates	Total Number of Samples per Experiment
Control	2	2	2	6
1	2	3 feed/3 filtrate	2 service cycles	14
2	2	3 feed/3 filtrate	2 service cycles	14
3	2	3 feed/3 filtrate	2 service cycles	14

##### 4.1.2 Seedings Using Activated Sludge

Four virus seedings were performed on the MBR pilot plant. These included two seedings at a low fouled condition, and additional seedings at medium and high fouled conditions. Two low-fouled virus seedings were performed after a chemical cleaning of the membrane using NaOCl. A description of the chemical cleanings performed is given in Appendix B. The membrane continued to foul as the system was operated, and a virus seeding was performed at medium and high-fouled conditions.

An MS-2 bacteriophage solution was injected into the primary effluent feed stream of the MBR pilot plant over an 8-hour period. The bacteriophage solution was sampled at the beginning and end of each seeding. (Table 4-2) Samples were collected once per hour from the influent stream

downstream of the virus injection and at the permeate of the membrane, 1 minute after the membrane backwashed. Prior to the study, literature review revealed that it was difficult to retrieve virus from samples collected containing activated sludge. After the first low-fouled virus seeding, samples were taken from the activated sludge and lab analyses showed good recovery of virus. Upon this discovery, samples were collected from the aeration basin for the remainder of the seedings.

**Table 4-2 Virus seeding solution concentration at the beginning and end of each seeding using activated sludge**

<b>Fouling Condition</b>	<b>Virus Solution Concentration, Initial (PFU/100 mL)</b>	<b>Virus Solution Concentration, Final (PFU/100 mL)</b>	<b>Concentration Change, Logarithmic</b>
Low-1	4.50E+09	3.00E+09	-0.18
Low-2	2.30E+09	5.00E+08	-0.66
Medium	2.40E+09	5.00E+08	-0.68
High	1.30E+10	3.00E+08	-1.64

#### ***4.1.3 Seedings Using Colorado River Water***

Like the testing conducted using the primary effluent wastewater, four virus seedings were also performed on the pilot plant using CRW. Two seedings were performed at low fouled condition, and as at a medium and high fouled condition using CRW. The two low-fouled virus seedings were performed after a chemical cleaning of the membrane. The membrane continued to foul as the system was operated, and a virus seeding was performed at a medium and high-fouled condition

MS-2 bacteriophage was seeded directly into the reactor 2 minutes before the seeding experiment began. The reactor concentration was sampled at the beginning, middle and end of two consecutive filtration cycles. The reactor concentration at the beginning and end of each seeding showed no significant change in concentration. (Table 4-3) Samples were collected at the feed and permeate over two consecutive filtration cycles 1 minute before backwash, 1 minute after backwash, and at the middle of the cycle.

**Table 4-3 Reactor concentration at the beginning and end of each seeding using Colorado river water**

<b>Fouling Condition</b>	<b>Reactor Concentration, Initial (PFU/100 mL)</b>	<b>Reactor Concentration, Final (PFU/100 mL)</b>	<b>Concentration Change, Logarithmic</b>
Low-1	4.30E+08	2.10E+08	-0.31
Low-2	2.50E+09	6.60E+08	-0.58
Medium	2.10E+08	2.70E+08	0.11
High	6.70E+08	7.70E+08	0.06

## 4.2 RESULTS OF VIRUS SEEDINGS USING ACTIVATED SLUDGE

### 4.2.1 Operating Parameters

The Zenon MBR pilot plant was operated in a nitrification only mode during the virus seeding experiments. The Zenon MBR was operated at a HRT of 4 hours and an average SRT of 10 days. The MLSS concentration was maintained at 8,000 mg/L. The membrane was agitated with continuous aeration using coarse air diffusers at a flowrate of 30 scfm. Table 4-4 shows the membrane operation during the virus seedings for the MBR pilot plant using activated sludge.

**Table 4-4 Operating conditons during virus seedings using activated sludge**

<b>Fouling Condition</b>	<b>Target Flux (gfd)</b>	<b>Vacuum Pressure (psi)</b>	<b>Specific Flux (gfd/psi)</b>
Low-1	19	1.76	10.80
Low-2	19	2.52	7.54
Medium	19	3.83	4.96
High	19	7.12	2.67

### 4.2.2 Seeding Results

Table 4-5 shows the results of the virus seedings performed on the Zenon MBR pilot plant using the primary effluent. A probability plot of the results of the virus seedings using activated sludge can be seen in Figure 4-1. The Zenon MBR achieved 3-log removal of viruses in 50% of samples from the feed to the permeate of the system. There was just over 2-log removal in 50% of all samples from the aeration basin to the effluent of the pilot plant.

**Table 4-5 Zenon MBR virus seeding results using activated sludge**

Time (h)	Fouling Condition	Feed Concentration (PFU/100 mL)	Sludge Concentration (PFU/100 mL)	Permeate Concentration (PFU/100 mL)	Log Removal (Feed to Permeate)	Log Removal (Sludge to Permeate)
0	Low-1	5.40E+07	NA	2.60E+04	3.32	NA
1	Low-1	4.40E+07	NA	6.60E+05	1.82	NA
2	Low-1	5.60E+07	NA	6.30E+05	1.95	NA
3	Low-1	6.40E+07	NA	8.50E+05	1.88	NA
4	Low-1	5.20E+07	NA	NA	NA	NA
5	Low-1	2.40E+07	NA	7.70E+05	1.49	NA
6	Low-1	3.90E+07	NA	6.90E+05	1.75	NA
7	Low-1	2.10E+07	NA	5.10E+05	1.61	NA
8	Low-1	2.40E+07	NA	3.80E+05	1.80	NA
0	Low-2	2.78E+08	4.00E+03	2.00E+02	6.14	1.30
1	Low-2	2.30E+07	7.20E+05	2.50E+05	1.96	0.46
2	Low-2	2.30E+07	7.54E+06	1.60E+05	2.16	1.67
3	Low-2	1.20E+07	1.70E+06	8.20E+04	2.17	1.32
4	Low-2	2.10E+07	2.90E+06	6.30E+04	2.52	1.66
5	Low-2	1.00E+07	2.00E+06	3.70E+04	2.43	1.73
6	Low-2	1.30E+07	2.80E+05	5.30E+04	2.39	0.72
7	Low-2	1.40E+07	3.00E+05	4.40E+04	2.50	0.83
8	Low-2	9.00E+06	2.80E+05	3.30E+04	2.44	0.93
0	Medium	2.70E+07	3.90E+04	1.00E+02	5.43	2.59
1	Medium	1.50E+07	2.00E+06	8.80E+03	3.23	2.36
2	Medium	2.60E+07	1.20E+06	8.40E+03	3.49	2.15
3	Medium	2.30E+07	1.30E+06	9.10E+03	3.40	2.15
4	Medium	1.30E+07	1.60E+06	8.30E+03	3.19	2.29
5	Medium	9.00E+06	1.70E+06	7.70E+03	3.07	2.34
6	Medium	1.90E+07	2.10E+05	9.20E+03	3.31	1.36
7	Medium	1.40E+07	1.80E+05	6.40E+03	3.34	1.45
8	Medium	5.40E+06	2.40E+05	6.20E+03	2.94	1.59
0	High	2.00E+07	1.00E+05	2.00E+01	6.00	3.70
1	High	2.30E+07	8.20E+05	5.50E+02	4.62	3.17
2	High	1.30E+07	1.70E+06	1.60E+03	3.91	3.03
3	High	5.90E+06	1.30E+06	2.20E+03	3.43	2.77
4	High	7.60E+06	2.00E+06	1.60E+03	3.68	3.10
5	High	6.40E+06	2.70E+06	1.30E+03	3.69	3.32
6	High	5.50E+06	1.50E+06	7.00E+02	3.90	3.33
7	High	1.80E+06	1.70E+06	8.00E+02	3.35	3.33
8	High	1.50E+06	1.40E+06	7.00E+02	3.33	3.30

Not Analyzed

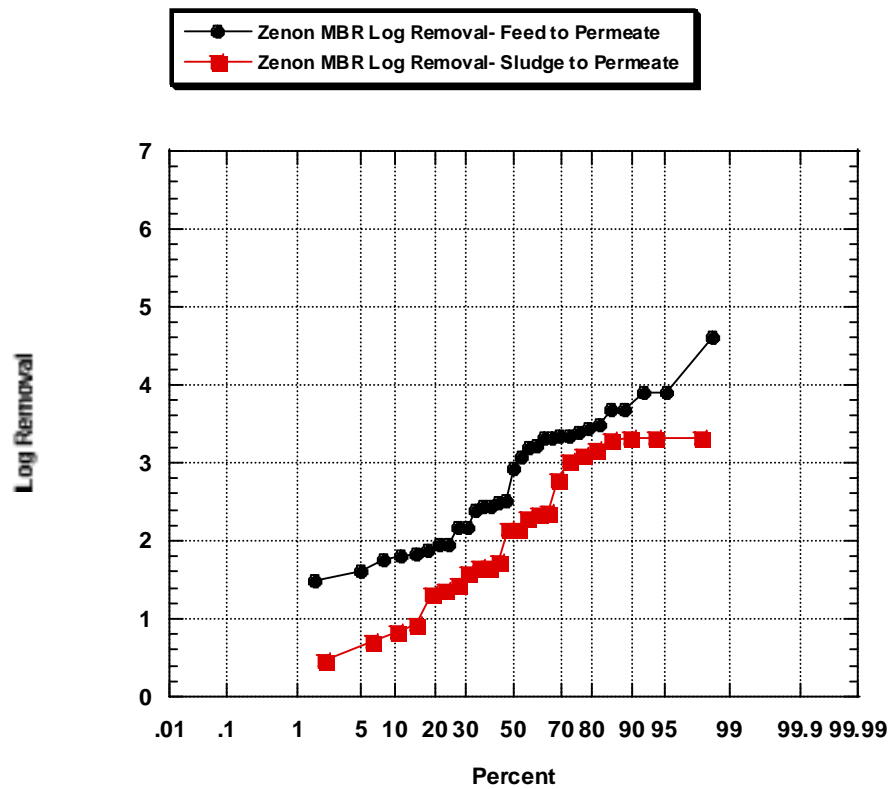
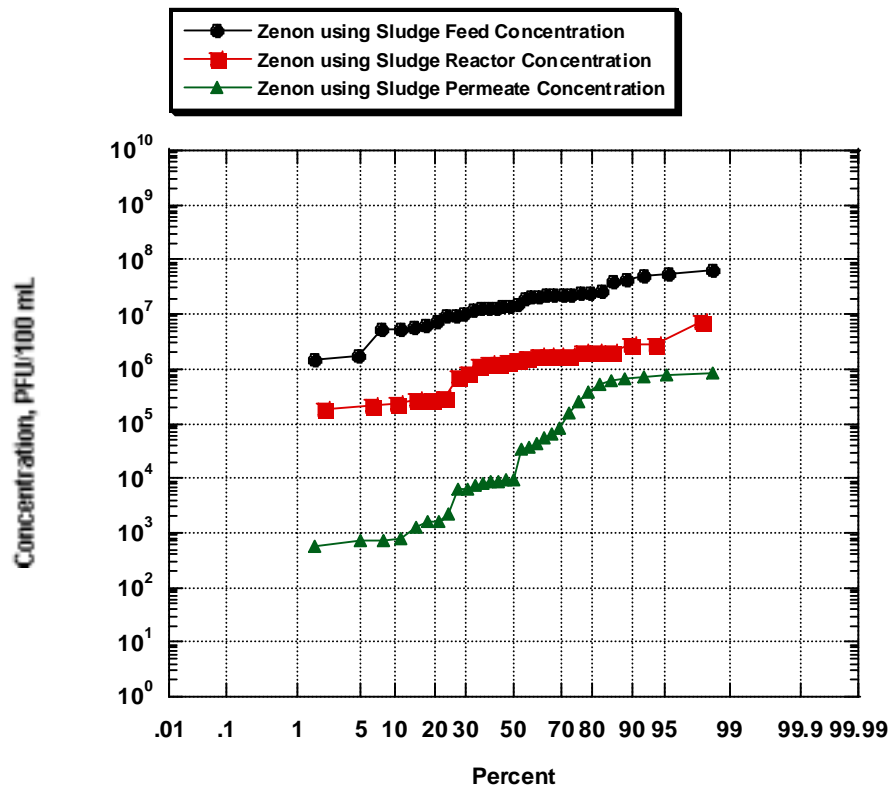


Figure 4-1 Probability plots of virus seedings of Zenon MBR using activated sludge

### 4.3 VIRUS SEEDINGS USING COLORADO RIVER WATER

#### 4.3.1 Operating Parameters

The Zenon MBR pilot plant was retrofitted to operate using CRW. The membrane was operated in the same manner as before. The pilot plant was operated in a dead-end fashion during all virus seedings, meaning a waste stream was not used. The membrane was agitated with continuous aeration using coarse air diffusers at a flowrate of 30 scfm. Table 4-6 shows the membrane operation during the virus seedings for the MBR pilot plant.

**Table 4-6      Operating Conditions during virus seedings using Colorado River Water**

<b>Fouling Condition</b>	<b>Target Flux (gfd)</b>	<b>Vacuum Pressure (psi)</b>	<b>Specific Flux (gfd/psi)</b>
Low-1	19	0.90	21.11
Low-2	19	0.93	20.43
Medium	19	2.04	9.31
High	19	2.97	6.40

#### 4.3.2 Seeding Results

Table 4-7 shows the results of the virus seedings performed on the Zenon MBR pilot plant using CRW. A probability plot of the results of the virus seedings using activated sludge can be seen in Figure 4-2. The Zenon MBR achieved >2-log removal in 50% of samples of virus from the reactor to the permeate of the system.

**Table 4-7 Zenon MBR virus seeding results using Colorado river water**

<b>Time (min)</b>	<b>Fouling Condition</b>	<b>Reactor Concentration (PFU/100 mL)</b>	<b>Permeate Concentration (PFU/100 mL)</b>	<b>Log Removal</b>
1	Low-1	4.30E+08	6.70E+06	1.81
5	Low-1	1.90E+08	3.00E+07	0.80
9	Low-1	2.30E+08	3.00E+07	0.88
1	Low-1	1.50E+08	9.00E+06	1.22
5	Low-1	2.70E+08	1.40E+07	1.29
9	Low-1	2.10E+08	1.80E+07	1.07
1	Low-2	2.50E+09	5.50E+07	1.66
5	Low-2	7.50E+08	4.80E+07	1.19
9	Low-2	6.60E+08	5.70E+07	1.06
1	Low-2	4.90E+08	5.60E+07	0.94
5	Low-2	5.20E+08	5.10E+07	1.01
9	Low-2	6.60E+08	5.50E+07	1.08
1	Medium	2.10E+08	3.30E+05	2.80
5	Medium	2.50E+08	1.90E+05	3.12
9	Medium	2.60E+08	2.00E+05	3.11
1	Medium	2.40E+08	3.40E+05	2.85
5	Medium	3.50E+08	3.20E+05	3.04
9	Medium	2.70E+08	1.90E+05	3.15
1	High	6.70E+08	2.50E+05	3.43
5	High	7.50E+08	6.70E+05	3.05
9	High	8.50E+08	8.00E+04	4.03
1	High	8.20E+08	1.30E+05	3.80
5	High	5.20E+08	8.10E+05	2.81
9	High	7.70E+08	1.00E+05	3.89



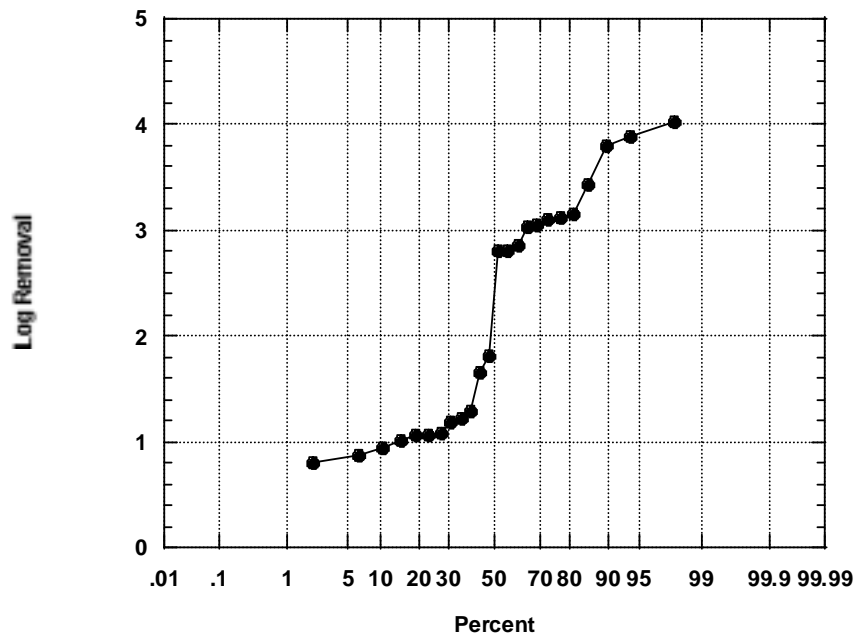
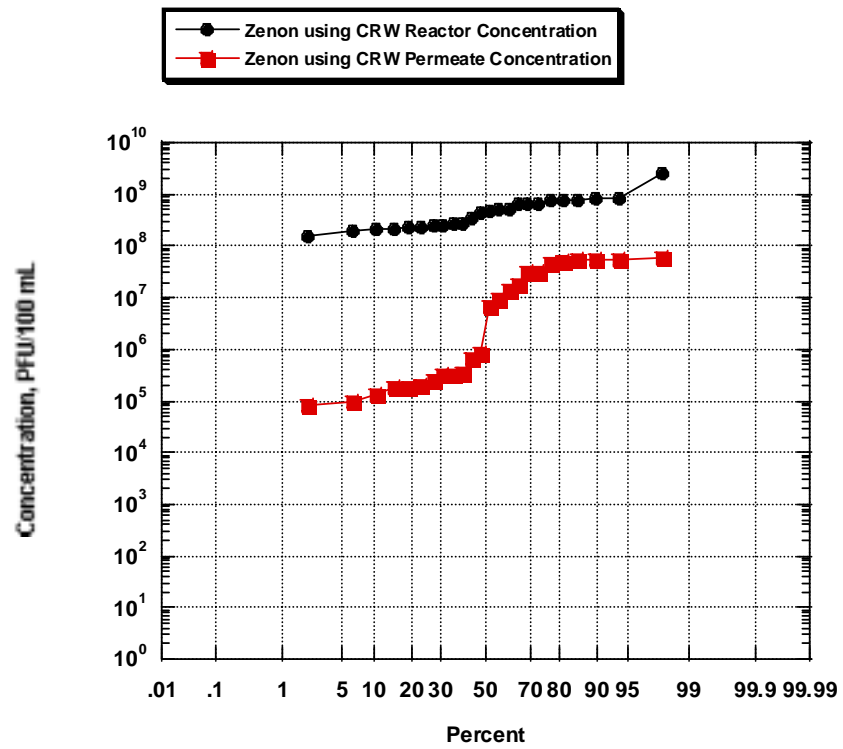


Figure 4-2 Probability Plots of Zenon MBR using Colorado river water

## **SECTION 5**

### **Regulatory Approval**

#### **5.1 INTRODUCTION**

Representatives from California and 5 additional State Regulatory Agencies were contacted and sent preliminary versions of this report. The representatives were requested to review the results presented in the report and respond in writing with regard to the ability of the MBR technology to meet applicable State wastewater recycling criteria. This section presents the results of this regulatory approval task.

#### **5.2 CALIFORNIA REGULATORY APPROVAL PROCESS**

In California, the latest version of the Water Recycling Criteria<sup>1</sup>, presents the following criteria for a filtered wastewater:

“Has been passed through a microfiltration, ultrafiltration, nanofiltration, or reverse osmosis membrane so that the turbidity of the filtered wastewater does not exceed any of the following:

- (1) 0.2 NTU more than 5 percent of the time within a 24-hour period; and
- (2) 0.5 NTU at any time.”<sup>2</sup>

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<sup>1</sup> Water Recycling Criteria. Proposed Regulations Water Recycling. R-13-95. Marked up version of the State criteria that is stamped “Received October 13, 1998: Drinking Water Program Santa Rosa District.” Title 22, Chapter 3, Article 1.

<sup>2</sup> In addition, the latest version of the State Water Recycling Criteria defines a disinfected tertiary recycled water as a filtered and subsequently disinfected wastewater that meets the following criteria:

- (a) The filtered wastewater has been disinfected by either:
  - (1) A chlorine disinfection process following conventional treatment or its equivalent that provides a CT (the product of total chlorine residual and modal contact time measured at the same point) value of not less than 450 milligram-minutes per liter at all times with a modal contact time of at least 90 minutes, based on peak dry weather design flow; or
  - (2) A disinfection process that, when combined with the filtration process, has been demonstrated to inactivate and/or remove 99.999 percent of the plaque-forming units of F-specific bacteriophage MS2, or polio virus in the wastewater. A virus that is at least as resistant to disinfection as polio virus may be used for purposes of the demonstration.
- (b) The medium concentration of total coliform bacteria measured in the disinfected effluent does not exceed an MPN of 2.2 per 100 milliliters utilizing the bacteriological results of the last seven days for

On March 2, 2000 MWH project team members and City of San Diego representatives met with representatives of the California DHS. In part, the goal of the meeting was to discuss data needed and the process to be followed to obtain DHS approval for using the MBR process to Title 22 Water Recycling Criteria.

DHS staff indicated that to obtain approval, Title 22 requires a 0.2 NTU effluent (never to exceed 0.5 NTU) combined with disinfection to achieve a total of 5 log removal of virus. In addition, DHS indicated that to obtain their approval, the MBR process would need to achieve a 1-log removal of virus (DHS indicated they would consider basing this virus credit on the 50<sup>th</sup> percentile of virus rejection). The minutes of the March 1, 2000 meeting with the representatives of California DHS are presented in Appendix A.

A letter was sent to Mr. Jeff Stone of the California DHS requesting conditional approval for use of the MBR under Title 22 water recycling criteria. In addition Mr. Stone received preliminary copies of this report. On April 23, 2001, Mr. Stone responded with a letter to Mr. Doug Thompson of Zenon Environmental, granting conditional approval for the use of their MBR for water recycling under Title 22. Copies of the request and acceptance letters are provided in Appendix C. The acceptance letter states:

“The demonstration studies conducted using the Zenon MBR have sufficiently demonstrated the ability to produce an oxidized wastewater and the membranes ability to comply with the above stated turbidity performance requirements. In addition, virus seeding experiments demonstrated the processes ability to achieve a 1-log virus reduction at the 50<sup>th</sup> percentile. Therefore, the Department of Health Services accepts the use of this membrane, identified as the Zenon MBR utilizing the OCP membrane, as a filtration technology for use in compliance with the Water Recycling Criteria. Based on performance data, the membrane filtration units will be limited to a maximum flux of 20 gfd and a maximum vacuum pressure of –8 psi.”

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which analyses have been completed and the number of total coliform bacteria does not exceed an MPN of 23 per 100 milliliters in more than one sample in any 30 day period. No sample shall exceed an MPN of 240 total coliform bacteria per 100 milliliters.”

In addition, the approval letter indicated that the DHS would review all projects on a case by case basis to determine full compliance with all treatment and reliability requirements.

### **5.3 ADDITIONAL CANDIDATE STATES**

After formally contacting DHS and requesting approval for use of MBR as an alternative to filtration to meet the Title 22 Wastewater Recycling Criteria, MWH contacted 5 additional states to seek regulatory approval or at least to obtain some kind of feedback from the State regulatory authority's as to the use of MBR technology to meet their wastewater recycling criteria.

Table 5-1 presents preliminary information obtained from contacting the selected States and reviewing their regulations, standards and criteria documents. The contacts at each State regulatory agency were sent a copy of a preliminary version of this report. In addition, they received a copy of the California DHS approval letter. A cover letter requested a review of the enclosed materials and a written response with respect to the ability of the Zenon MBR technology to meet the State's regulatory requirements. The letters sent to State Regulators are presented in Appendix D. The responses received from the five States are provided as Appendix E and summarized below.

#### *5.3.1 Arizona*

A response was received from Gregory H. Brown, P.E, Wastewater Design Review Unit Manager for the Arizona Department of Environmental Quality (ADEQ) in a letter dated August 21, 2001. The letter states "the Zenon MBR appears to meet the effluent requirements for Class A reclaimed water in accordance with AAC R18-9-303 and the treatment performance requirements found in AAC R19-9-B204." It also states that "the Zenon MBR does not appear to meet the total nitrogen criteria of 10 mg/L found in AAC R18-9-B204." The letter states that the ADEQ does not provide individual product review approvals, but only provides technical review of technology when it is included as a component in an entire system designed for installation. The letter also states that "the ADEQ does not provide product review approvals,"

but rather “provides technical review when it is included as a component of an entire designed system.”

**Table 5-1 Overview of State Wastewater Reuse Information**

	Contact	Agency Name	Reuse Regulations	Criteria (most stringent)
Arizona	Natasha Mu	Department of Environmental Quality	Title 18: Environmental Quality, Article 7 Regulations for Reuse of Wastewater	Food Consumed Raw (fecal coliform 2.2/100 mL, geo mean, no single sample >25/100 mL; 1 NTU, 1 virus per 40 L, no detectable entamoeba, giardia, ascaris, tapeworm)
Florida	David York, Ph.D.	Department of Environmental Protection	Chapter 62-610, Reuse of Reclaimed Water and Land Application	[Discharge to Class 1 surface water used for potable supply] No detectable fecal coliform/100 mL, 5 mg/L TSS, 20 mg/L CBOD, 10 mg/L NO <sub>3</sub> (as N). Meet primary and secondary drinking water standards.
Texas	Louis Herrin	Texas Natural Resource Conservation Commission	Chapter 210, 210.1-210.9	Type 1 Reclaimed Water Use (BOD <sub>5</sub> or COD <sub>5</sub> at 5 mg/L, turbidity of 3 NTU, fecal <20/100 mL (geo. mean); fecal <75/100 mL (single grab sample)
Oregon	Walt West	Department of Environmental Quality	Deivision 55, Regulations Pertaining to the Use of Reclaimed Water (Treated Effluent) from Sewage Treatment Plants	2.2/100 mL 7-day median total coliforms, 23/100 mL maximum coliform, 2 NTU, 24 hour max 5 NTU, 5% of time during 24 hours
Washington	Kathy Cupps	Department of Ecology	Water Reclamation and Reuse Standards	Direct recharge into potable gw aquifer (oxidation, filtration, RO, disinfection) drinking water MCLs, turbidity <0.1 NTU, nitrogen <10 mg/L, TOC <1.0 mg/L, turbidity <2 NTU, total coliforms 1/100 mL median of previous 7 days, 5/100 mL maximum.

### *5.3.2 Florida*

A response was received from David W. York, Ph.D. P.E, reuse coordinator for the Florida State Department of Environmental Protection in a letter dated July 3, 2001. The letter listed the reclaimed water requirements for Florida and indicated that the State does not approve specific products, but instead reviews processes on a case-by-case basis during the Department's review of permit applications. The letter went on to state that "the performance of the Zenon system was encouraging" and that "the well-conceived study yielded a wealth of valuable information". The system met turbidity requirements, would most likely met TSS requirements based on the low turbidity, (TSS was not measured), had no detectable fecal coliforms in 95 percent of samples and exceed 6 logs removal of fecal coliforms in about 70 percent of samples, and achieved a 50<sup>th</sup> percentile of 2.1 logs removal of MS2 virus.

### *5.3.3 Texas*

The Texas Natural Resource Conversation Commission did not respond to the approval request letter, after repeated requests.

### *5.3.4 Oregon*

The Oregon Department of Environmental Quality informed us in an email dated July 28, 2001 that they would not be providing comments on the Zenon MBR process due to work loads and time restrictions.

### *5.3.5 Washington*

A response was received from Kathy Cupps, P.E, Ecology Water Reclamation Lead Engineer for the Washington State Department of Ecology in a letter dated July 3, 2001. The letter stated the following:

1. The Ecology Department does not approve proprietary technologies, but rather each individual reclamation facility design is reviewed in accordance with the specific application.
2. When the Ecology Department has not established standards for new technology, it looks for justification from other State experiences. In Ms. Cupps opinion, the membrane standards of

California State Title 22 could be considered as appropriately conservative for the filtration step in Washington State Class A reclaimed water.

3. In Ms. Cupps opinion, the NWRI study would satisfy the requirements of a Class A equivalent filtration technology for water reclamation facilities that would propose to use of MBR technology.
4. This approval would be contingent on membrane and wastewater characteristics at the proposed facility that do not deviate substantially from the membrane and wastewater characteristics for the NWRI study.
5. The NWRI study does not fully demonstrate Ecology's requirement for nitrogen reduction when reclamation facilities discharge to ground water via surface percolation. The total nitrogen as N maximum is 10 mg/L in this case.
6. Ms. Cupps would like to see more information on operations and maintenance costs, ease of cleaning procedure, required level of operator skill, and long-term operating viability. She states that perhaps the experience at the Arapahoe, Colorado facility would provide this.

A second reviewer at Washington State was Craig Riley, P.E. In addition to reiterating many of Ms. Cupps observations, Mr. Riley indicated that MBR could result in a reduction in the disinfection step required for Class A reclaimed water. The details of this reduction are presented in Mr. Rileys written response titled "DOH comments July, 2001, Membrane Bioreactor Recognition – Mitsubishi and Zenon," presented in Appendix E.

## **SECTION 6**

### **Summary and Conclusions**

#### **6.1 BUREAU OF RECLAMATION STUDY**

In October 1998 the City of San Diego was awarded a grant from the Bureau of Reclamation to evaluate the MBR process and its potential application to wastewater reclamation. During Part 1 of the study the system was operated in a nitrification/denitrification mode using an auxiliary anoxic tank. During Part 2, the pilot plant was operated in a nitrification only mode. The primary objectives of the Bureau of Reclamation project were to obtain long-term operational and performance data for the MBR process in treating primary wastewater effluent.

The Bureau of Reclamation study demonstrated the following:

- The MBR pilot system was capable of producing a good quality effluent water suitable for use by an RO system.
- Run times between chemical cleanings were reasonable.
- Very high removal of total and fecal coliforms and total coliphage was achieved.
- Excellent organic removal was achieved.
- The Zenon MBR pilot system achieved complete nitrification and partial denitrification during Part 1, and complete nitrification during Part 2.

In a meeting with California DHS personnel in March 2000, DHS indicated that in order for California to consider the MBR process for a formal approval from the State that virus seeding studies would also be needed. In addition, the DHS indicated that approval would in part be based on the MBR's ability to demonstrate at least a 1-log removal of MS-2 virus at the 50<sup>th</sup> percentile.

#### **6.2 VIRUS SEEDING STUDY**

As requested by DHS, virus seeding studies were conducted using both primary effluent wastewater and Colorado River Water as the feed to the MBR. Four seedings were conducted using each feed water. Two of the seedings were conducted at low fouled conditions, one at



medium fouled condition and one at a high fouled condition. Samples were taken from the MBR permeate, the MBR feed water and the activated sludge. Sludge concentrations were approximately 1 log lower than feed water concentrations because of lower recovery of the organism from sludge samples. Log removals of virus were calculated based on both feed water and sludge concentrations. The 50<sup>th</sup> percentile log removal of MS-2 exceeded 2 logs in all cases, thus exceeding the DHS requirement of 1 log removal

### **6.3 REGULATORY APPROVAL**

State regulators from California and 5 other States were requested to review the MBR operational and virus seeding results presented in a preliminary version of this report and provide a written response with regard to the MBR ability to meet State wastewater reclamation criteria. The individual responses are summarized below.

#### *6.3.1 California*

Mr. Jeff Stone, Chief of the Water Recycling Unit at the California DHS was sent a letter requesting approval of the Zenon MBR process as an acceptable filtration technology under California Title 22. In a letter dated April 23, 2001, Zenon Environmental received notification from the California DHS that the studies conducted sufficiently demonstrated the Zenon MBR ability to comply with State Recycling Criteria as a filtration technology under Title 22. The MBR permeate met all turbidity requirements and demonstrated greater than 1-log removal of seeded MS2 virus. Further the DHS stipulated that the acceptance was granted specifically for the ZeeWeed®-OCP UF membrane, operating at a flux no greater than 20 gfd and a maximum vacuum pressure of -8 psi.

#### *6.3.2 Arizona*

The Arizona response letter states “the Zenon MBR appears to meet the effluent requirements for Class A reclaimed water in accordance with AAC R18-9-303 and the treatment performance requirements found in AAC R19-9-B204.” It also states that “the Zenon MBR does not appear to meet the total nitrogen criteria of 10 mg/L found in AAC R18-9-B204.”

### 6.3.3 *Florida*

The Florida response letter states that “the performance of the Zenon system was encouraging” and that “the well-conceived study yielded a wealth of valuable information”. The system met turbidity requirements, would most likely met TSS requirements based on the low turbidity, (TSS was not measured), had no detectable fecal coliforms in 95 percent of samples and exceed 6 logs removal of fecal coliforms in about 70 percent of samples, and achieved a 50<sup>th</sup> percentile of 2.1 logs removal of MS2 virus.

### 6.3.4 *Texas*

No response was received from Texas.

### 6.3.5 *Washington*

The Washington response letter indicated the following.

- The membrane standards of California State Title 22 could be considered as appropriately conservative for the filtration step in Washington State Class A reclaimed water.
- The NWRI report would satisfy the requirements of a Class A equivalent filtration technology for water reclamation facilities that would propose to use of MBR technology.
- The NWRI report does not fully demonstrate Ecology’s requirement for nitrogen reduction when reclamation facilities discharge to ground water via surface percolation. The total nitrogen as N maximum is 10 mg/L in this case.
- The State would like to see more information on operations and maintenance costs, ease of cleaning procedure, required level of operator skill, and long-term operating viability.

Regulators from every State but California indicated they do not approve proprietary technologies. All States indicated they would review individual reclamation facility designs in accordance with their ability to meet the requirements of a specific application.

The responses received from California and the additional states are encouraging. The information exchanged with these states could provide a strong foundation for greater acceptance, approval and use of the MBR technology in these and other states across the country.

## SECTION 7

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**APPENDIX A**  
**MEETING MINUTES**

# MEMORANDUM



Aqua 2000 Research Center  
14103 Highland Valley Road  
Escondido, California 92025

**Date:** 3/2/00

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**To:** Samer Adham, PhD

**From:** Rion Merlo and Shane Trussell

**Subject:** Meeting Minutes

---

Subject: California Department of Health Services visit to the Aqua 2000 Research Center to discuss the results from the MBR pilot testing and MBR process compliance with Title 22.

Attendees:

Samer Adham	(MWH)
Daniel Askenaizer	(MWH)
Brian Bernados	(California Department of Health Services)
Paul Gagliardo	(City of San Diego)
Edward Hitti	(California Department of Health Services)
Rion Merlo	(MWH)
Toby Roy	(California Department of Health Services)
Rick Sakaji	(California Department of Health Services)
Jeff Stone	(California Department of Health Services)
Rhodes Trussell	(MWH)
R. Shane Trussell	(MWH)
Jeff Williams	(City of San Diego)

WELCOME AND INTRODUCTIONS:

Paul Gagliardo: The purpose of this MBR testing has been to investigate the operation and cost-effectiveness of the MBR process and to investigate the feasibility of getting Title 22 approval for the MBR process to use the product water as reclaimed water. The Metro Waste Water Department is close to making a decision about replacing the existing treatment system at San Pasqual with an MBR process.

PRESENTATION OF BUREAU OF RECLAMATION RESULTS:

Samer Adham presented data from the Bureau of Reclamation funded project, "Membrane Bioreactors for Water Reclamation." The issue of coliform breakthrough in the Zenon MBR was discussed. Possibilities of permanent pore blocking and possible contamination of the piping were discussed, however the point was continually highlighted that the process is still getting

much better removals than a tertiary filtration step. Samer indicated that the testing of the MBR process would be shut down by the end of March 2000.

With regard to the coliform results the project team indicated that the membrane is not an absolute barrier. However, from the data, it appears that when the UF was installed the high total coliforms are only residual growth in the line from the previous run with the MF membrane.

DHS agreed with this observation. From the data, the fecal coliforms dropped to non-detect immediately after the installation of the UF (OCP) membrane. It appears that the total coliforms are only residual.

The project team observed that there is only a slight chance that the total coliform are due to residual growth because they made a concerted effort to eliminate all contamination issues. The permeate line was chlorinated twice per week with 200 ppm of free chlorine for an hour, not counting the full chemical cleans. In fact, a micro sample was collected immediately after the membrane, before going through any piping. Possibly, there's a dead spot in the line where the coliform could still grow, but it is highly unlikely that it did not get disinfected.

During the discussion that followed, the project team indicated that they have reason to believe that the Zenon membrane used in wastewater is made from the same material as the drinking water membrane, but it does not have the same pore distribution as the drinking water membrane. The manufacturer has indicated that they are the same membrane.

The DHS indicated that if that were the case, then it is not the same membrane. DHS indicated a concern with regard to manufacturing issues that were discussed, and stated that their position is to be very strict on manufacturing issues.

The project team observed that this raises an important issue regarding how to regulate membrane manufacturing, and that currently there is no such process in place.

The discussion moved to obtaining Title 22 approval. DHS indicated that Title 22 requires a 0.2 NTU effluent turbidity combined with disinfection to achieve a total of 5 log removal of virus. To get DHS approval, the MBR would need to achieve a 1-log removal of virus.

The project team suggested that we could test the MBRs by feeding poliovirus to the systems and adding a disinfection unit (chlorine contactor or UV disinfection) after the MBR. We could monitor the influent and effluent for poliovirus in order to determine if the system could achieve 5-log removal of virus. We could also spike the influent with MS-2 phage and see if we can recover any from the primary effluent. Another suggestion was that the testing could use Colorado aqueduct water spiked with phage. This would represent a "worst-case" testing scenario for the MBR process.

The project team, however, also observed that such testing will be unfair to the "MBR process". The Mitsubishi MF will not provide one log removal of virus (based upon the 95<sup>th</sup> percentile) when challenged in a "solids-free" environment. If this is the case and the Mitsubishi MBR does not achieve the required virus reduction for Title 22 approval, this could leave only one potential manufacturer for the full-scale bid.

The DHS indicated that could consider basing virus credit on the 50<sup>th</sup> percentile of virus rejection.

The project team indicated that during the remainder of the month of March, they will conduct testing for the purposes of obtaining Title 22 approval for the MBR.

DHS discussed the process for submitting the proposal to obtain Title 22 approval to the Water Reclamation Committee (proposals could either be submitted in writing with supporting documentation, or a presentation could be made to the committee.)

At the end of the meeting, DHS requested information on the status of the n-Nitrosodimethylamine (NDMA) testing? Previously, the project team indicated that there would be sampling for NDMA conducted as part of this project. The project team indicated that MWH Laboratories has resolved issues with regard to the analytical method and that samples for NDMA will be collected this week. The current action level has been set at 20 ppt (initially the action level had been set at 2 ppt, but was recently raised by DHS as part of an investigation as to whether or not NDMA is a disinfection byproduct).

As an additional action item, DHS requested that Zenon must provide a written statement that the wastewater/water OCP membranes are identical.

#### ACTION ITEMS

1. MWH will contact Zenon, and request that they provide a written statement to Jeff Stone, DHS, indicating that the water OCP membrane and the wastewater OCP membrane are the same membrane and are manufactured using the same procedures.
2. MWH will conduct testing with the goal of obtaining virus reduction results for Title 22 approval.



**APPENDIX B**  
**CHEMICAL CLEANING PROCEDURE**

### **Zenon Chlorine Cleaning Protocol**

Chemical Reagent: NaOCl (effective chlorine concentration: 2,000 mg/L)

Volume of Chemical Reagent: 1.35 L/ft<sup>2</sup> of membrane area

1. Isolate the ZenoGem tank
2. Drain tank, and hose down until water appears clear
3. Fill with tap water
4. Add chlorine solution to the ZenoGem tank
5. Circulate the cleaning solution through the membrane
6. Close appropriate valves to prevent water from siphoning out through the membrane
7. Allow to soak overnight
8. Drain tank and hose down until there is no chlorine present
9. Put back into service

### **Zenon Citric Acid Cleaning Protocol**

Chemical Reagent: Citric Acid (effective pH = 2.5)

1. Isolate the ZenoGem tank
2. Drain tank, and hose down until water appears clear
3. Fill with tap water
4. Add citric acid solution to the ZenoGem tank
5. Circulate the cleaning solution through the membrane
6. Close appropriate valves to prevent water from siphoning out through the membrane
7. Allow to soak overnight
8. Drain tank and hose down until there is no citric acid present
9. Put back into service

## **APPENDIX C**

### **CALIFORNIA REQUEST AND ACCEPTANCE LETTERS**



January 17, 2001

Mr. Jeff Stone  
Department of Health Services  
1180 Eugenia Place, Suite 205  
Carpinteria, CA 93010-2000

Re: Request for Zenon MBR Approval under Title 22 Water Recycling Criteria

Dear Mr. Stone:

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)." In October 1998 the City of San Diego was awarded a grant from the Bureau of Reclamation to evaluate the MBR and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon Environmental Inc. MBR.

Montgomery Watson is requesting DHS approval of the Zenon Membrane Bioreactor (MBR) filtration unit as acceptable filtration technology for compliance with the California Wastewater Reclamation Criteria (Title 22). Based on the results obtained during the Bureau of Reclamation funded study the Zenon Environmental Inc. MBR process met the turbidity performance criteria (presented in the latest version of the Title 22 reclamation criteria) as well as the virus reduction performance criteria discussed at our meeting March 1, 2000 in San Diego.

For your consideration, we have enclosed a draft letter recognizing the performance of the Zenon Environmental Inc. MBR and indicating DHS approval of this process as an acceptable filtration technology for compliance with the California Wastewater Reclamation Criteria (Title 22).

Please let me know if we can provide you with any additional information. Thank you in advance for your consideration of this request.

Sincerely,

Samer Adham, Ph.D.  
Montgomery Watson

SA/rl

Enclosure

DEPARTMENT OF HEALTH SERVICES  
DIVISION OF DRINKING WATER AND ENVIRONMENTAL MANAGEMENT  
TECHNICAL OPERATIONS SECTION  
RECYCLED WATER UNIT  
1180 Eugenia Place, Suite 200  
Carpinteria, CA 93013  
(805) 566-9787  
FAX (805) 566-4780



April 23, 2001

Mr. Doug Thompson, P.E.  
Wastewater Process Manager  
Zenon Environmental Systems, Inc.  
3239 Dundas Street West  
Oakville, Ontario L6M 4B2  
Canada

Subject: Use of the Zenon MBR to comply with California  
Water Recycling Criteria

Dear Mr. Thompson:

By letter dated March 22, 2001, Montgomery Watson requested Departmental approval of the Zenon Membrane Bioreactor (MBR) filtration treatment unit as an acceptable filtration technology for compliance with the State of California Water Recycling Criteria (Title 22). Accompanying this request was a report prepared by Montgomery Watson and the City of San Diego entitled "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental, Inc.)", dated March 2001. This report was prepared for the National Water Research Institute. The Department has reviewed this report and offers the following comments.

The Zenon MBR filtration system evaluated utilizes the "ZeeWeed®-OCP UF" membrane with a nominal pore size of 0.035 micron. The membranes are submerged and are operated in the dead-end mode under vacuum pressure with a maximum design flux of 20 gallons per square foot per day (gfd).

The California Water Recycling Criteria recognize membrane filtration as an acceptable filtration technology provided prescribed performance requirements (i.e. turbidity) are reliably met. The turbidity performance criteria require that the filtered wastewater not exceed any of the following:

1. 0.2 NTU more than 5 percent of the time within a 24-hour period; and

2. 0.5 NTU at any time


The demonstration studies conducted using the Zenon MBR have sufficiently demonstrated the ability to produce an oxidized wastewater and the membranes ability to comply with the above stated turbidity performance requirements. In addition, virus seeding experiments demonstrated the processes ability to achieve a 1-log virus reduction at the 50<sup>th</sup> percentile. Therefore, the Department of Health Services accepts the use of this membrane, identified as the Zenon MBR utilizing the OCP membrane as a filtration technology for use in compliance with the Water Recycling Criteria. Based on performance data, the membrane filtration units will be limited to a maximum flux of 20 gfd and a maximum vacuum pressure of -8 psi.

The acceptance of your technology is specific to the Zenon ZeeWeed®-OCP UF membrane having a nominal pore size of 0.035 micron. Any proposed changes made in the physical attributes or character of this membrane shall be reviewed in advance by the Department to determine whether the modifications will require additional testing.

The Department will continue to review all proposed projects on a case-by-case basis to determine full compliance with all applicable treatment and reliability features required by the Water Recycling Criteria. This will include the collective review of all treatment unit processes, operational controls (e.g. loading rates, TMP, frequency of integrity tests), 'O&M' procedures, etc.

If you have any questions concerning this letter, please contact the undersigned at (805) 566-9767.

Sincerely,



Jeffrey L. Stone, Chief  
Recycled Water Unit  
Division of Drinking Water

cc: ✓Montgomery Watson - Samer Adham  
National Water Research Institute - Ron Linsky  
City of San Diego - Paul Gagliardo  
Recycled Water Committee

**APPENDIX D**

**ADDITIONAL STATE REVIEW REQUESTS**

## **Arizona**





June 18, 2001

FILE	
Client #:	_____
File #:	_____
Job #:	_____

Mr. Greg Brown  
Wastewater Design Unit Manager  
Arizona Department of Environmental Quality  
3033 North Central Ave  
Phoenix, AZ 85012

**Re: Request for Zenon MBR Recognition Under AAC Section R18-11-303**

Dear Mr. Brown,

On June 13, 2001 you spoke with Dr. Dan Askenaizer of Montgomery Watson regarding the issue of State recognition of membrane bioreactor technology as capable of producing an effluent meeting specific reclamation criteria contained in the Arizona Administrative Code. This letter is being sent to you as a followup to that discussion.

Earlier this year California's Department of Health Services (DHS) recognized in a letter that the Zenon MBR technology (as tested) can produce an effluent meeting the requirements of the State's water reclamation criteria. DHS was careful, however, to indicate that they will continue to review the application of the MBR technology on a case-by-case, project-by-project basis. The National Water Research Institute (NWRI) is interested in purposing similar types of feedback from State regulatory agencies around the US. NWRI thus funded this effort which is being managed by Montgomery Watson. NWRI has funded numerous studies with the goal of promoting the use of water reclamation technology.

After a discussion with Marcie Mullins of the Arizona DEQ, the same information that was sent to the California DHS for their review was sent to Mr. Asif Majeed (cover letter dated May 10, 2001). Per your request we are sending the same information as sent to Mr. Majeed to your attention. If possible, we would like to receive a formal response from the State of Arizona (like what was provided by California DHS) regarding the ability of the MBR technology to meet specified effluent criteria. If that is not possible, we would appreciate any guidance you could provide as to how and under what procedures the State would review the application of such technology.

What follows below is the text of the letter to Mr. Majeed. Thank you in advance for your consideration and any response that you can provide.

## **Introduction**

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental, Inc.)." In October 1998 the City of San Diego and Montgomery Watson were awarded a grant from the Bureau of Reclamation to evaluate the Membrane Bioreactor (MBR) and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon MBR. A second, smaller study, funded by the National Water Research Institute, is building upon the efforts of the Bureau of Reclamation study to conduct a more in-depth evaluation of state regulatory issues associated with the MBR process. Part of this effort includes contacting individual State regulatory agencies and requesting their review of the enclosed material.

## **California DHS Review**

During the Bureau of Reclamation funded study initial contacts were made with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process. During those discussions, DHS staff requested additional data showing the ability of the MBR process to remove viruses. As part of the NWRI study, therefore, virus seeding experiments were conducted to provide that needed information. The virus seeding studies are described in the enclosed report. The enclosed report was submitted to the California DHS with the request for approval of the MBR technology as meeting the State's water reclamation criteria for filtration.

After reviewing the enclosed information the California DHS has written a letter recognizing that the MBR technology is an acceptable filtration technology for use in meeting the State's Water Recycling Criteria. A copy of the letter from Mr. Jeff Stone of the California Department of Health Services (DHS) is also enclosed. Mr. Stone can be reached at (805) 566-9767.

## **Request for ADEQ Review**

Montgomery Watson is requesting a review and response from the Arizona Department of Environmental Quality (ADEQ) that the Zenon MBR filtration is an acceptable "alternative treatment method" for compliance with Arizona Administrative Code, Section R18-11-303 Class A+ Reclaimed Water (Section R18-11-303(A)-R18-11-303(C)).

According to Section R18-11-303(B)-(C), a Class A+ reclaimed water must meet the following requirements:

1. The turbidity of the reclaimed water effluent prior to disinfection must meet a 24-hour turbidity of 2 NTU or less, never to exceed 5 NTU.
2. After disinfection the effluent must have no detectable fecal coliforms in 4 of the last 7 daily samples and the single maximum must be below 23/100 mL.

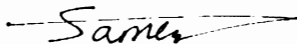
3. If an alternative process is used, there must be no detectable enteric virus in 4 of the last 7 monthly samples.
4. The 5-sample geometric mean concentration of total nitrogen in a reclaimed water is less than 10 mg/L.
5. Alternative treatment may be used (other than secondary treatment, filtration, nitrogen removal and disinfection) provided there is a demonstration through pilot plant testing, water quality data or other means that the reclaimed water effluent meets the disinfection criteria and the total nitrogen criteria.

Based on the results obtained during the Bureau of Reclamation funded study, and the additional virus removal challenge studies that are presented in the enclosed report, we believe the Zenon MBR process met the turbidity performance criteria, the disinfection performance criteria, the nitrogen performance criteria as well as the virus reduction performance criteria.

If you believe this enclosed information is adequate, Montgomery Watson and the NWRI would like to request a formal response from ADEQ recognizing that MBR is capable of producing a Class A+ reclaimed water as described in Arizona Administrative Code Section R18-11-303. We recognize that any approved use of the MBR technology on a given reclamation project within the State must go through a formal review and approval process to determine compliance with all applicable treatment and reliability requirements.

Please let me know if we can provide you with any additional information. I can be reached at (626) 568-6751. Thank you in advance for your consideration of this request.

Sincerely,



Samer Adham, Ph.D.  
Montgomery Watson

cc w/o enclosures

Ron Linsky (NWRI)  
Doug Thompson (Zenon)  
Dan Askenaizer (Montgomery Watson)

Enclosures

**Florida**



**MONTGOMERY WATSON**  
Applied Research Department

May 10, 2001

Dr. David York  
Reuse Coordinator  
Florida Department of Environmental Protection  
Tallahassee, FL 32399-2400

**Re: Request for Recognition of MBR Performance Per State Reclamation Criteria**

Dear Dr. York,

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)." In October 1998 the City of San Diego and Montgomery Watson were awarded a grant from the Bureau of Reclamation to evaluate the Membrane Bioreactor (MBR) and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon MBR. A second, smaller study, funded by the National Water Research Institute, is building upon the efforts of the Bureau of Reclamation study to conduct a more in-depth evaluation of state regulatory issues associated with the MBR process. Part of this effort includes contacting individual State regulatory agencies and requesting their review of the enclosed material.

**California DHS Approval of MBR Technology**

During the Bureau of Reclamation funded study initial contacts were made with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process. During those discussions, DHS staff requested additional data showing the ability of the MBR process to remove viruses. As part of the NWRI study, therefore, virus seeding experiments were conducted to provide that needed information. The virus seeding studies are described in the enclosed report. The enclosed report was submitted to the California DHS with the request for approval of the MBR technology as meeting the State's water reclamation criteria for filtration.

After reviewing the enclosed information the California DHS has written a letter recognizing that the MBR technology is an acceptable filtration technology for use in meeting the State's Water Recycling Criteria. A copy of the letter from Mr. Jeff Stone of the California DHS is also enclosed. Mr. Stone can be reached at (805) 566-9767.

**Request for Florida DEP Review of MBR Results**

Montgomery Watson is requesting a formal response from the Florida Department of Environmental Protection (DEP) that the Zenon MBR filtration is capable of producing an effluent water that meets the quality criteria specified in the Florida Administrative

Code Section 62-610.460 Waste Treatment and Disinfection and Section 62-600.440(5) on high-level disinfection.

According to Section 62-610.460 the reclaimed water effluent shall contain less than 5 mg/L of suspended solids. The section goes on to state that "Filtration shall be provided for TSS control. Chemical feed facilities for coagulant, coagulant aids, or polyelectrolytes shall be provided. Such chemical feed facilities may be idle if the TSS limitation is being achieved without chemical additional.....Filtration also serves as the primary barrier for removal of protozoan pathogens (Cryptosporidium, Giardia and others)."

According to Section 62-600.440(5) facilities should provide additional TSS control (beyond secondary treatment levels) and shall be designed to result in a reclaimed water in which fecal coliform values are below detectable limits.

If you believe this enclosed information is adequate, Montgomery Watson and the NWRI would like to request a formal response from Florida DEP recognizing that MBR is capable of producing a reclaimed water meeting the requirements contained in Sections 62-610.460 and 62-600.440(5). We recognize that any approved use of the MBR technology on a given reclamation project within the State must go through a formal review and approval process to determine compliance with all applicable treatment and reliability requirements.

Please let me know if we can provide you with any additional information. I can be reached at (626) 568-6751. Thank you in advance for your consideration of this request.

Sincerely,



Samer Adham, Ph.D.  
Montgomery Watson

cc w/o enclosures  
Ron Linsky (NWRI)  
Doug Thompson (Zenon)  
Dan Askenaizer (Montgomery Watson)

Enclosures

## **Oregon**



May 17, 2001

Ms. Judy Johndohl  
Municipal Wastewater Specialist  
Oregon Department of Environmental Quality  
811 SW 6th Street  
Portland, OR 97204

**Re: Request for Zenon MBR Recognition**

Dear Ms. Johndohl,

I regret that recently you and Dan Askenaizer have been unable to talk prior to my sending you this letter. Given the short timeframe for our project with the National Water Resources Institute (NWRI) I have decided to go ahead and send you this information and request. We are sending this information to a number of states across the country.

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)." In October 1998 the City of San Diego was awarded a grant from the Bureau of Reclamation to evaluate the Membrane Bioreactor (MBR) and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon MBR. A second, smaller study, funded by the National Water Research Institute, is building upon the efforts of the Bureau of Reclamation study to conduct a more in-depth evaluation of state regulatory issues associated with the MBR process. Part of this effort includes contacting Individual State regulatory agencies and requesting their review of the enclosed material.

**California DHS Review**

During the Bureau of Reclamation funded study initial contacts were made with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process. During those discussions, DHS staff requested additional data showing the ability of the MBR process to remove viruses. As part of the NWRI study, therefore, virus seeding experiments were conducted to provide that needed information. The virus seeding studies are described in the enclosed report. The enclosed report was submitted to the California DHS with the request for approval of the MBR technology as meeting the State's water reclamation criteria for filtration.

After reviewing the enclosed information the California DHS has written a letter recognizing that the MBR technology is an acceptable filtration technology for use in



meeting the State's Water Recycling Criteria. A copy of the letter from Mr. Jeff Stone of the California Department of Health Services (DHS) is also enclosed. . Mr. Stone can be reached at (805) 566-9767.

### **Request for Oregon DEQ Review**

Montgomery Watson is requesting a review and response from the Oregon Department of Environmental Quality that the Zenon MBR technology is an acceptable filtration technology to meet the intent of section 340-055-0015 (4)(a) of Division 55 (Regulations Pertaining to the Use of Reclaimed Water (treated Effluent) from Sewage Treatment Plants) wherein it states the following:

“Where Table 1, for specified uses, requires that reclaimed water receive biological, coagulation, clarification, filtration treatment plus disinfection, the Department will consider treatment processes that do not utilize coagulation provided that equivalent effluent quality to that achieved with coagulation can be demonstrated. (emphasis added) The Department shall consult with the Oregon Health Division when considering alternative treatment processes allowed for under this section.”

Based on the results obtained during the Bureau of Reclamation funded study and the additional virus removal challenge studies that are presented in the enclosed report we believe the Zenon MBR process met the turbidity performance criteria (contained in section 340-055-0010(14) definition of filtration), and the coliform limits described in Table 1 in Division 55 (Regulations Pertaining to the Use of Reclaimed Water (Treated Effluent) from Sewage Treatment Plants).

If you believe this enclosed information is adequate, Montgomery Watson and the NWRI would like to request a formal response from Oregon Department of Environmental Quality recognizing that MBR is capable of producing effluent quality equivalent to the requirements for filtration technology using coagulation as described in the Oregon Administrative Code. We recognize that any approved use of the MBR technology on a given reclamation project within the State must go through a formal review and approval process to determine compliance with all applicable treatment and reliability requirements.

Please let me know if we can provide you with any additional information. I can be reached at (626) 568-6751. Thank you in advance for your consideration of this request.

Sincerely,



Samer Adham, Ph.D.  
Montgomery Watson

cc w/o enclosures

Ron Linsky (NWRI)

Doug Thompson (Zenon)

Dan Askenaizer (Montgomery Watson)

Enclosures

**Texas**



**MONTGOMERY WATSON**  
Applied Research Department

May 10, 2001

Mr. Louis Herrin  
TNRCC, MC-148  
P.O. Box 13087  
Austin, TX 78711

Texas Natural Resource Conservation Commission

**Re: Request for Zenon MBR Recognition Under AAC Section R18-11-303**

Dear Mr. Herrin,

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)." In October 1998 the City of San Diego and Montgomery Watson were awarded a grant from the Bureau of Reclamation to evaluate the Membrane Bioreactor (MBR) and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon MBR. A second, smaller study, funded by the National Water Research Institute, is building upon the efforts of the Bureau of Reclamation study to conduct a more in-depth evaluation of state regulatory issues associated with the MBR process. Part of this effort includes contacting individual State regulatory agencies and requesting their review of the enclosed material.

**California DHS Review**

In addition a copy of the letter received from Mr. Jeff Stone of the California Department of Health Services (DHS) is also enclosed. During initial contacts with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process, DHS staff requested additional data showing the ability of the MBR process to remove viruses. As part of the NWRI study, therefore, virus seeding experiments were conducted to provide that needed information and are described in the enclosed report. The letter from Mr. Stone of DHS grants the Zenon MBR conditional approval for use in California. Mr. Stone can be reached at (805) 566-9767.

**Request for TNRCC Review**

Montgomery Watson is requesting a formal response from the Texas Natural Resource Conservation Commission (TNRCC) that the Zenon MBR filtration can produce an effluent water that meets the quality criteria specified in Chapter 210-Use of Reclaimed

Water, Subchapter C, Section 210.33 (1) Quality Standards for Using Relcaimed Water in the Texas Administrative Code..

According to Section 210.33 (1) Quality Standards for Using Relcaimed Water reclaimed water must meet the following requirements for a Type I recliamed water use (based on a 30-day average):

1. BOD5 or CBOD5 of 5 mg/L
2. Turbidity of 3 NTU,
3. Fecal Coliform of 20 cfu/100 mL (geometric mean)
4. Fecal Coliform (not to exceed) 75 cfu/100 mL (single grab sample)

Based on the results obtained during the Bureau of Reclamation funded study and presented in the enclosed report the Zenon MBR process met the turbidity performance criteria, the disinfection performance criteria, the nitrogen performance criteria as well as the virus reduction performance criteria.

Please let me know if we can provide you with any additional information. I can be reached at (626) 568-6751. Thank you in advance for your consideration of this request.

Sincerely,



Samer Adham, Ph.D.  
Montgomery Watson

cc w/o enclosures

Ron Linsky (NWRI)  
Doug Thompson (Zenon)  
Dan Askenaizer (Montgomery Watson)

Enclosures

**Washington**



**MONTGOMERY WATSON**  
Applied Research Department

May 10, 2001

Ms. Kathy Cupps, P.E.  
Water Reclamation and Reuse Lead  
Washington Department of Ecology  
P.O. Box 47600  
Olympia, WA 98504-7600

**Re: Request for Zenon MBR Recognition**

Dear Ms. Cupps,

Please find enclosed a copy of the report "Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)." In October 1998 the City of San Diego and Montgomery Watson were awarded a grant from the Bureau of Reclamation to evaluate the Membrane Bioreactor (MBR) and its potential application to wastewater reclamation. This report includes a summary of the results and observations from the study conducted using the Zenon MBR. A second, smaller study, funded by the National Water Research Institute, is building upon the efforts of the Bureau of Reclamation study to conduct a more in-depth evaluation of state regulatory issues associated with the MBR process. Part of this effort includes contacting individual State regulatory agencies and requesting their review of the enclosed material.

**California DHS Approval of MBR Technology**

During the Bureau of Reclamation funded study initial contacts were made with representatives of the California Department of Health Services (DHS) on regulatory requirements for the MBR process. During those discussions, DHS staff requested additional data showing the ability of the MBR process to remove viruses. As part of the NWRI study, therefore, virus seeding experiments were conducted to provide that needed information. The virus seeding studies are described in the enclosed report. The enclosed report was submitted to the California DHS with the request for approval of the MBR technology as meeting the State's water reclamation criteria for filtration.

After reviewing the enclosed information the California DHS has written a letter recognizing that the MBR technology is an acceptable filtration technology for use in meeting the State's Water Recycling Criteria. A copy of the letter from Mr. Jeff Stone of the California DHS is also enclosed. Mr. Stone can be reached at (805) 566-9767.

## **Request for Review by Washington Department of Ecology**

Montgomery Watson is requesting a formal response from the Washington Department of Ecology that the Zenon MBR filtration is capable of producing an effluent water that meets the language provided in the Water Reclamation and Reuse Standards (September 1997) for a Class A reclaimed water.

Specifically, the Washington State Water Reclamation and Reuse Standards provides the following definitions:

**Class A Reclaimed Water** – means reclaimed water that, at a minimum, is at all times an oxidized, coagulated, filtered, disinfected wastewater. The wastewater shall be considered adequately disinfected if the median number of total coliform organisms in the wastewater after disinfection does not exceed 2.2 per 100 milliliters, as determined from the bacteriological results of the last 7 days for which analyses have been completed, and the number of total coliform organisms does not exceed 23 per 100 milliliters in any sample.

The requirements of a Class A reclaimed water is addressed in the additional definitions presented below that are contained within the Water Reclamation and Reuse Standards:

**Coagulated Wastewater** – means an oxidized wastewater in which colloidal and finely divided suspended matter have been destabilized and agglomerated prior to filtration by the addition of chemicals or by an equally effective method.

**Disinfected wastewater** means wastewater in which pathogenic organisms have been destroyed by chemical, physical or biological means.

**Filtered Wastewater** – means an oxidized, coagulated wastewater which has been passed through natural undisturbed soils or filter media, such as sand or anthracite, so that the turbidity as determined by an approved laboratory method does not exceed an average operating turbidity of 2 nephelometric turbidity units (NTU), determined monthly, and does not exceed 5 NTU at any time.

**Oxidized Wastewater** means wastewater in which organic matter has been stabilized such that the biochemical oxygen demand (BOD) does not exceed 30 mg/L and the total suspended solids (TSS) do not exceed 30 mg/L, is nonputrescible, and contains dissolved oxygen.

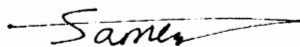
Based on the results obtained during the Bureau of Reclamation funded study and the virus seeding study presented in the enclosed report on the Zenon MBR, we believe the effluent from the MBR process would meet the definition of a Class A reclaimed water.



If you believe this enclosed information is adequate, Montgomery Watson and the NWRI would like to request a formal response from Washington Department of Ecology recognizing that MBR is capable of producing a Class A reclaimed water as described in the state's Water Reclamation and Reuse Standards . We recognize that any approved use of the MBR technology on a given reclamation project within the State must go through a formal review and approval process to determine compliance with all applicable treatment and reliability requirements.

Please let me know if we can provide you with any additional information. I can be reached at (626) 568-6751. Thank you in advance for your consideration of this request.

Sincerely,



Samer Adham, Ph.D.  
Montgomery Watson

cc w/o enclosures

Ron Linsky (NWRI)

Doug Thompson (Zenon)

Dan Askenaizer (Montgomery Watson)

Enclosures

**APPENDIX E**

**ADDITIONAL STATE RESPONSES**

## **Arizona**



James D. Hall  
Commissioner

# ARIZONA DEPARTMENT OF ENVIRONMENTAL QUALITY

1033 North Central Avenue • Phoenix, Arizona 85012-2000  
(602) 207-2300 • [www.adeq.state.az.us](http://www.adeq.state.az.us)



Josephine L. Aguilar  
Director

August 21, 2001

Samer Adham, Ph.D.  
Montgomery Watson  
250 N. Madison Ave  
Pasadena, CA 91101

RE: Zenon Membrane Bioreactor (MBR)

Dear Mr. Adham:

The Arizona Department of Environmental Quality (ADEQ) has received your request, dated June 18, 2001, for Zenon MBR recognition under Arizona Administrative Code R18-9-303 for Class A+ reclaimed water. Attached to the request was a report prepared by Montgomery Watson entitled *Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)*, March 2001. The report was prepared for the National Water Research Institute.

ADEQ does not provide product review approvals. ADEQ only provides technical review of technology when it is included as a component of an entire system designed for installation at a specific site under an aquifer protection permit in accordance with Arizona Administrative Code (AAC), Title 18, Chapter 9. However, review of the information presented in the report indicates that the Zenon MBR appears to meet the effluent requirements for Class A reclaimed water in accordance with AAC R18-9-303 and the treatment performance requirements found in AAC R18-9-B204. The Zenon MBR does not appear to meet the total nitrogen criteria of 10 mg/l found in AAC R18-9-B204.

If you have any questions or comments, please call me at 602-207-4697, or toll free in Arizona at 800-234-5677, extension 4697.

Sincerely,

Gregory H. Brown, P.E.  
Wastewater Design Review Unit Manager  
Water Permits Section  
Water Quality Division

RRP/01-2283

Northern Regional Office  
1515 East Cactus Avenue • Suite 1 • Flagstaff, AZ 86004  
(928) 779-0111

Southern Regional Office  
100 West Congress Street • Suite 421 • Tucson, AZ 85701  
(520) 698-0700

**Florida**



Jeb Bush  
Governor

# Department of Environmental Protection

Twin Towers Office Building  
2600 Blair Stone Road  
Tallahassee, Florida 32399-2400

David B. Struhs  
Secretary

July 3, 2001

Dr. Samer S. Adham  
Montgomery Watson  
250 N Madison Avenue  
Pasadena, CA 91101

Dear Dr. Adham:

Per your request, I reviewed the March 2001 report *Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)*. The Zenon membrane bioreactor (MBR) uses submerged membranes having nominal pore size of 0.035 microns. My comments follow:

On page 30, the report notes that Florida's most stringent reclaimed water limits are for discharges to Class I surface waters. Actually, the most stringent criteria are applied to ground water recharge projects that feature injection of reclaimed water to ground water having total dissolved solids (TDS) of 3,000 mg/L or less. This type of reuse system is regulated under Rule 62-610.560, Florida Administrative Code (F.A.C.). For this class of injection, the reclaimed water must meet the full treatment and disinfection requirements contained in Rule 62-610.563(3), F.A.C. A copy of Chapter 62-610, F.A.C., is enclosed for your reference. Reclaimed water must meet the primary and secondary drinking water standards (except for asbestos), a total nitrogen limit, and limits on total organic carbon and total organic halogen. Multiple barriers are required for control of organics and pathogens. We require that total suspended solids (TSS) be reduced by filtration below 5.0 mg/L as a single sample maximum before disinfection. We use total coliforms as our bacteriological indicator and require that no more than one sample be positive for total coliforms during a month and that no sample shall exceed 4 per 100 mL.

Part III of Chapter 62-610, F.A.C., regulates reclaimed water used to irrigate residential properties, public access areas, and edible crops. Filtration and high-level disinfection is required. High-level disinfection is defined in Rule 62-600.440(5), F.A.C. Filtration is required to reduce TSS below 5.0 mg/L as a single sample maximum before disinfection. Fecal coliforms are used as our indicator organism. At least 75 percent of observations of fecal coliforms must be below detection and no sample may exceed 25 per 100 mL.

Florida does not approve or endorse specific products or processes for wastewater treatment or water reclamation. Proposed projects and the unit processes involved are reviewed on a case-by-case basis during the Department of Environmental Protection's

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review of permit applications. Hence, my comments on the Zenon MBR do not constitute any form of state approval or endorsement.

This well-conceived study yielded a wealth of valuable information on the Zenon MBR system. The performance of the Zenon system was encouraging.

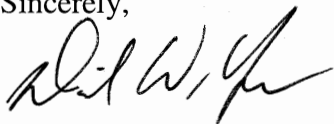
BOD<sub>5</sub> was reduced to less than 3 mg/L in 95 percent of the samples taken.

Turbidity was reduced to less than 0.1 NTU in 99 percent of the observations. Unfortunately, TSS data were not included in the report. Hence, the ability of the process to meet Florida's 5.0-mg/L TSS limit cannot be directly addressed. However, given the excellent performance related to turbidity, it is likely that this system would be able to meet the single sample maximum TSS limit of 5.0 mg/L.

Removals of fecal coliforms also were excellent. More than 95 percent of fecal coliform observations were less than 2 per 100 mL and log removals of fecal coliforms exceeded 6 logs in about 70 percent of observations. Virus removals (based on seeded trials using MS-2 bacteriophage) showed a fair amount of variability. The membranes removed 1.3 logs or less of MS-2 (reactor to permeate) in 20 percent of the observations. The 50-percentile log removal was about 2.1 logs. Removals exceeded 3 logs in about 30 percent of the observations. In general, virus removals increased as the degree of fouling increased. No data was presented on removal of the protozoan pathogens (notably Giardia and Cryptosporidium). As noted in our rules, there is growing interest in the protozoan pathogens in Florida. Proposals for implementation of alternative disinfection systems probably would need to be supported with virus and protozoan data in addition to documentation of the process' ability to meet Florida's coliform limits.

If you would like to discuss my comments or Florida's reuse criteria further, please call me at 850/922-2034. I can also be reached by e-mail at [david.york@dep.state.fl.us](mailto:david.york@dep.state.fl.us).

Sincerely,



David W. York, Ph.D., P.E.  
Reuse Coordinator

Enclosures

cc: Ron Linsky – NWRI  
Sharon Sawicki – DEP  
Elsa Potts – DEP

## **Oregon**





WEST.Walt@deq.state.or.us on 07/28/2001 12:37:08 AM

To: Daniel.askenaizer@mw.com  
cc:

Subject:

Daniel, The Oregon DEQ will not be providing comments on the membrane activated sludge process that was submitted on your behalf. Due to work loads and time restrictions we are limited to reviewing these processes as they are proposed on a case by case basis.

Thank You,  
Walt West, P.E.  
ER -Bend Office  
Bend, Oregon

**Texas**

**Washington**



## **DEPARTMENT OF ECOLOGY ENGINEERING/TECHNICAL REVIEW COMMENTS**

<b>Date:</b>	<b>July 3, 2001</b>
<b>To:</b>	<b>Samer Adham, Ph.D. Montgomery Watson</b>
<b>cc:</b>	<b>Craig Riley, P.E. Washington Department of Health Water Reclamation Lead Engineer</b>
<b>From:</b>	<b>Kathy Cupps, P.E. Ecology Water Reclamation Lead Engineer</b>
<b>Project:</b>	<b>Membrane Bioreactor Equivalency Determination</b>
<b>Prepared For:</b>	<b>National Water Research Institute Study</b>

Craig Riley and I have received and reviewed the following reports which were submitted to my attention in May, 2001.

1. Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Mitsubishi Rayon Co., Ltd.)
2. Assessing the Ability of Membrane Bioreactor to Meet Existing Water Reuse Criteria (Zenon Environmental Inc.)

We also received copies of the review conducted by the California Department of Health Services and your request to make a Class A equivalency determination for the membrane bioreactor technology. A copy of Mr. Riley's comments is attached. My comments are noted below.

1. Ecology does not approve proprietary technologies, per se. Each individual design is reviewed by the assigned engineer in accordance with the specific application. Ecology review includes engineering reports, plans and specifications and operation and maintenance manuals for reclaimed water facilities.
2. Ecology establishes or adopts minimum design criteria for technologies within our Criteria for Sewage Works Design, Publication No. 98-37 WQ (CSWD). Where criteria have not been established, Ecology looks for justification in standard engineering references. The CSWD discusses membrane technologies briefly in Chapter T4-2.6.1. Although specific design criteria for membrane treatment systems are not established in the CSWD, the following factors are required to be considered in evaluating membrane design.
  - a. Flux rate
  - b. Reject rate or recovery rate
  - c. Transmembrane operating pressure
  - d. Fouling rate
  - e. Backwashing or chemical cleaning capabilities
  - f. Overall operating costs including membrane replacement, power, chemicals for cleaning and labor

3. By definition, any technology which has not been incorporated into the CSWD is considered a new technology. The first step of the approval process is full-scale or representative pilot installations. To the extent that the NWRI data and test results meet the CSWD objectives noted below, the information can be considered as the submittal to satisfy Ecology's data submission requirements for membrane reactor technology.
  - a. All procedures used in validating the process are conducted under the supervision of a registered professional engineer experienced in sanitary engineering.
  - b. Sample data must demonstrate effectiveness and efficiency under minimum and maximum design conditions and over extended periods of time for the planned facility.
  - c. The data must be from continuous operation of a full-scale or pilot operation treating the type and strength of sewage to be handled.
  - d. Total flow and other process control measurements must be taken and recorded daily or at a frequency required to verify operation of the technology.
  - e. All analyses are made in accordance with the latest version of the EPA guidelines, 40 CFR 136 or "Standard Methods for the Examination of Water and Wastewater" by an accredited laboratory unless specifically approved by Ecology.
4. Upon completion of the engineering review for the specific project, Ecology grants an provisional approval for construction and a subsequent evaluation period between 12 and 18 months. Additional monitoring and testing may be required to adequately demonstrate performance. Upon successful completion of the provisional period, Ecology will grant full approval for operation. If operation is not successful, Ecology will require corrective action to assure the permit requirements are consistently achieved.
5. When standards are not established by Ecology, our agency looks for justification from other states experiences. Our standards were modeled in part after California standards. The membrane standards in Title 22 could be considered as appropriately conservative for the filtration step in our Class A reclaimed water.
6. It is my opinion, that the NWRI study would satisfy the requirements as a Class A equivalent filtration technology for water reclamation facilities that would propose use of the membrane bioreactor technology. It is important to note that the data provided is specific to the membranes and wastewater characteristics used in the study and cannot not be generalized to membranes with different specifications or wastewaters that deviate substantially from the pilot.
7. One important criteria that was not fully demonstrated is Ecology's requirement for nitrogen reduction when reclamation facilities discharge to ground water via surface percolation or land apply at levels above agronomic rates. In these cases, the total nitrogen as N (sum of organic N, ammonia, nitrite and nitrate) is limited to a maximum of 10 mg/L. Since the pilot was not designed to removal nitrogen below ten, this could possibly be satisfied with the use of appropriate selector technology or a stripping tower.
8. My immediate concerns are with operation and maintenance and the overall O&M costs of these facilities. Specifically, I am concerned with membrane fouling, ease of cleaning

procedures and the level of operator skill that may be required. Furthermore, the relatively short-term experiences of the pilot cannot answer the longer-term operating viability. Perhaps this can be supplemented by the experience of other facilities such as the Arapahoe facility in Colorado.

9. Mr. Riley's review for the Department of Health proposes a possible reduction to our CT requirement for chlorine disinfection. Ecology would defer to Health on the issue of appropriate disinfection for public health protection.

## DOH comments July, 2001

### Membrane Bioreactor Recognition - Mitsubishi & Zeon

As requested, I have reviewed both of the documents submitted to the State of California for recognition that these two MBR products conform to California Title 22 requirements for membrane filtration. Based on the information provided, it would appear to me that membrane filtration provides treatment that is basically equivalent to the filtration portion required of Class A Reclaimed Water, and could result in a reduction in the disinfection step required for Class A reclaimed water. Based on these challenge studies, I would propose that additional disinfection to provide a minimum of an additional four -log virus inactivation, which would make this approach equivalent to the California standards requiring 99.999 % inactivation of viruses.

Based on the USEPA Surface Water Treatment Rule Guidance Manual, Appendix E, four-log virus inactivation by free chlorine in a pH range of 6 to 9 would require the following CT's:

Temperature °C	CT Required, mg-min/L	Time at C = 1.0 ppm, minutes	Time at C = 0.5 ppm, minutes
0.5	12	12	24
5	8	8	16
10	6	6	12
15	4	4	8
20	3	3	6
25	2	2	4

This would in effect reduce the thirty-minute detention time identified in the standards in Section 1, Article 9, Section 5, to eight to 12 minutes under extreme cold conditions, while providing an equivalent level of disinfection. The contact time in the USEPA SWTRGM is based on the effective detention time as being identified as the  $T_{10}$  time based on a tracer study, which is not equivalent to the modal time determined by a tracer study, but could be related. The requirement to use a 90 minute contact time based on the modal time from the tracer study would seem to be much more conservative than providing 8 to 12 minutes based on  $T_{10}$  contact time.

The California compliance letters also continue review of proposed projects on a case-by-case basis to assure compliance with applicability and treatment reliability.

Technologically, it appears that membrane filtration will provide treatment equivalent to Class A reclaimed water standards, based on the assessment of turbidity and microbiologic reduction. The applicability of this process for nitrogen reduction is not considered. Nitrogen reduction is a concern in surface percolation, as the standards require nitrate less than 10 ppm, nitrogen reduction and compliance with non-degradation standards for groundwater quality. This must be determined by Department of Ecology, which has the expertise for this.

Approval for a proposal should require the MBR be accompanied by additional disinfection. To be conservative, the additional disinfection should comply with California Standards until an assessment of the basis for this standard is completed. At that time, the final determination

should go to the Technical Advisory Committee for review if the assessment supports CT's that are lower than the California standard.

Compliance statements issued by California also limit the design flux rate and establish a nominal pore size in the compliance acceptance. Other parameters that appear to be of interest include the specific flux rate, air scour rate, and the production / backwash cycle periods. Any case-by-case approval should address these issues, and require that at least the design flux rate for a nominal pore size be consistent with the California compliance protocol.

Finally, the case-by-case approvals in California will address operational controls such as loading rates, TMP, frequency of integrity tests and O&M procedures. Research and experience with these issues is necessary for adequate review and approval.